

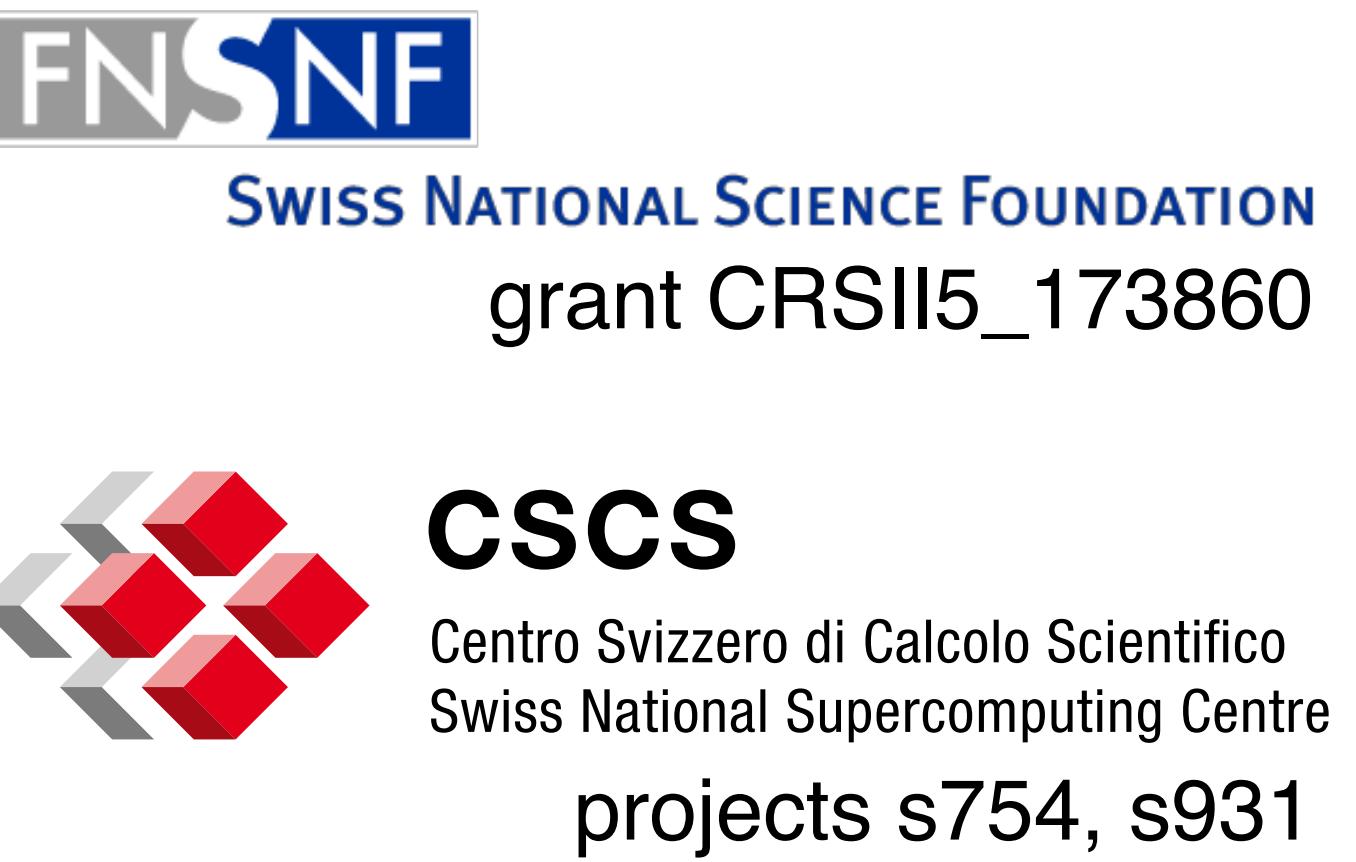
# **A High Performance Computing Framework for Multiphase, Turbulent Flows on Structured Grids**

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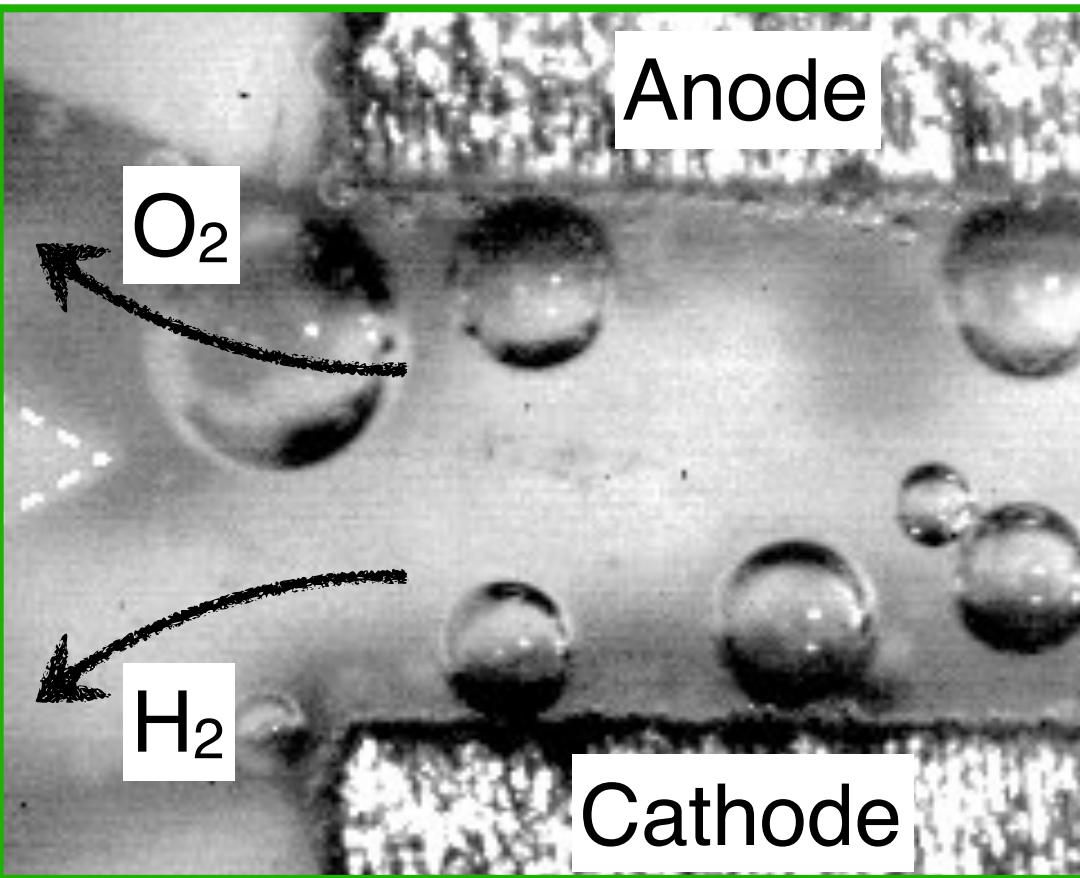
## **With:**

Fabian Wermelinger  
Michail Chatzimanolakis  
Dr. Sergey Litvinov  
Prof. Petros Koumoutsakos

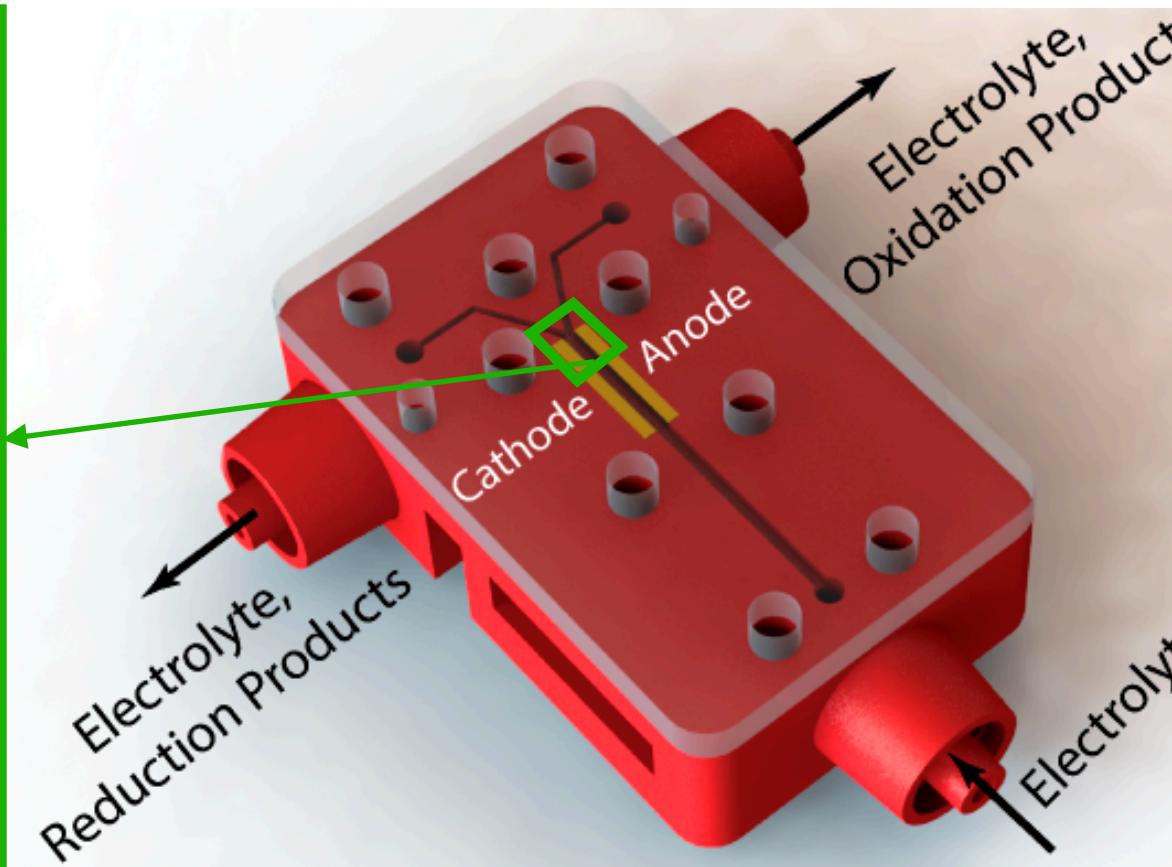


# Multiphase flows

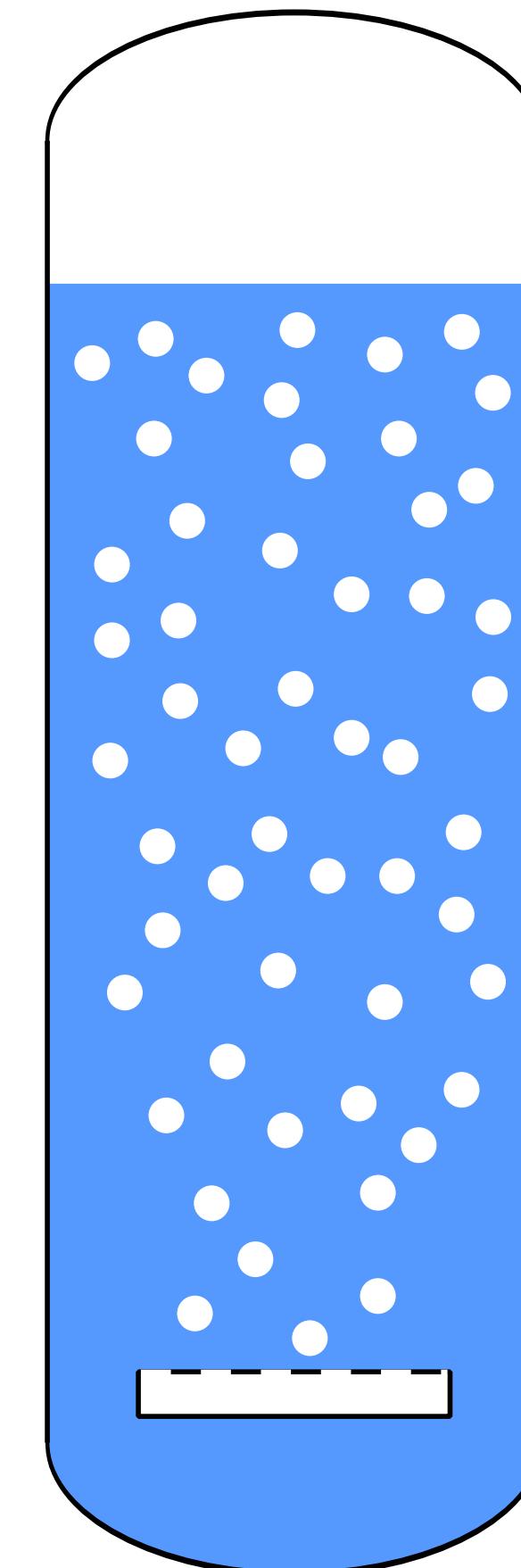
## Electrochemical cells



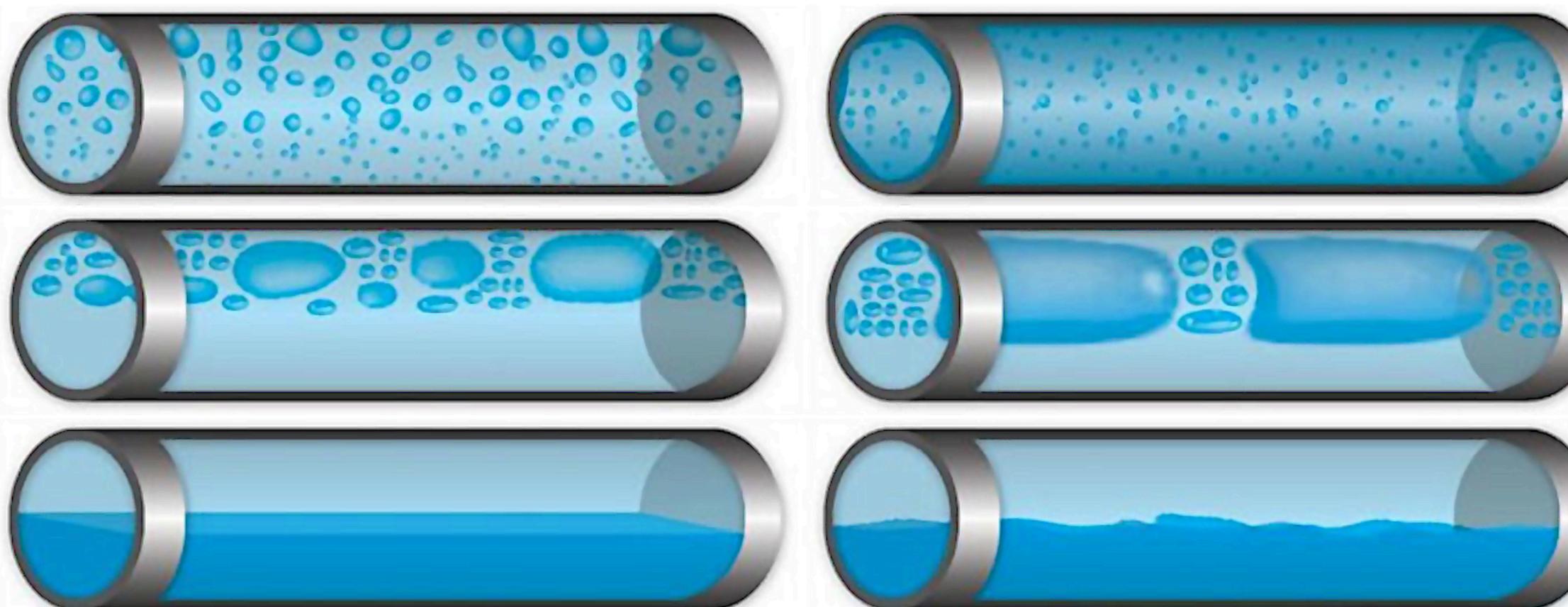
[Hashemi 2019]



## Bubble column reactors



## Pipes



[Bratland 2010]

[wikipedia]

# Outline

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## Numerical model

- new method for curvature estimation  
improving the accuracy at low resolution

## Implementation

- blockwise processing with coroutines for modularity

## Test cases

- curvature of a sphere
- translating droplet

## Applications

- bubble coalescence
- Taylor-Green vortex with bubbles
- plunging jet with air entrainment

# Numerical model

# Model

## Two-phase incompressible flow

- Navier-Stokes equations

$$\nabla \cdot \mathbf{u} = 0$$

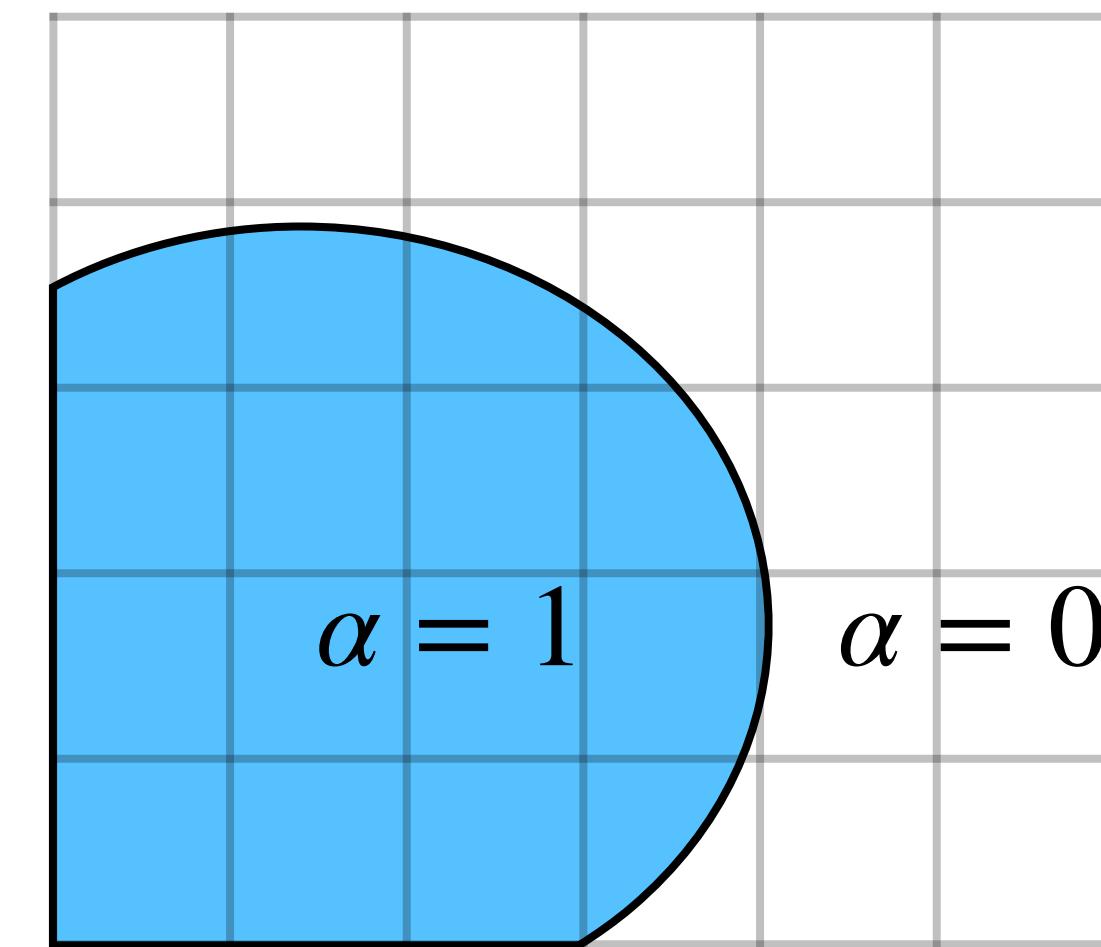
$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{u} \right) = -\nabla p + \nabla \cdot (\mu(\nabla \mathbf{u} + \nabla \mathbf{u}^T)) + \mathbf{f}_\sigma$$

- Advection of volume fraction

$$\frac{\partial \alpha}{\partial t} + (\mathbf{u} \cdot \nabla) \alpha = 0$$

$$\rho = (1 - \alpha)\rho_1 + \alpha\rho_2$$

$$\mu = (1 - \alpha)\mu_1 + \alpha\mu_2$$

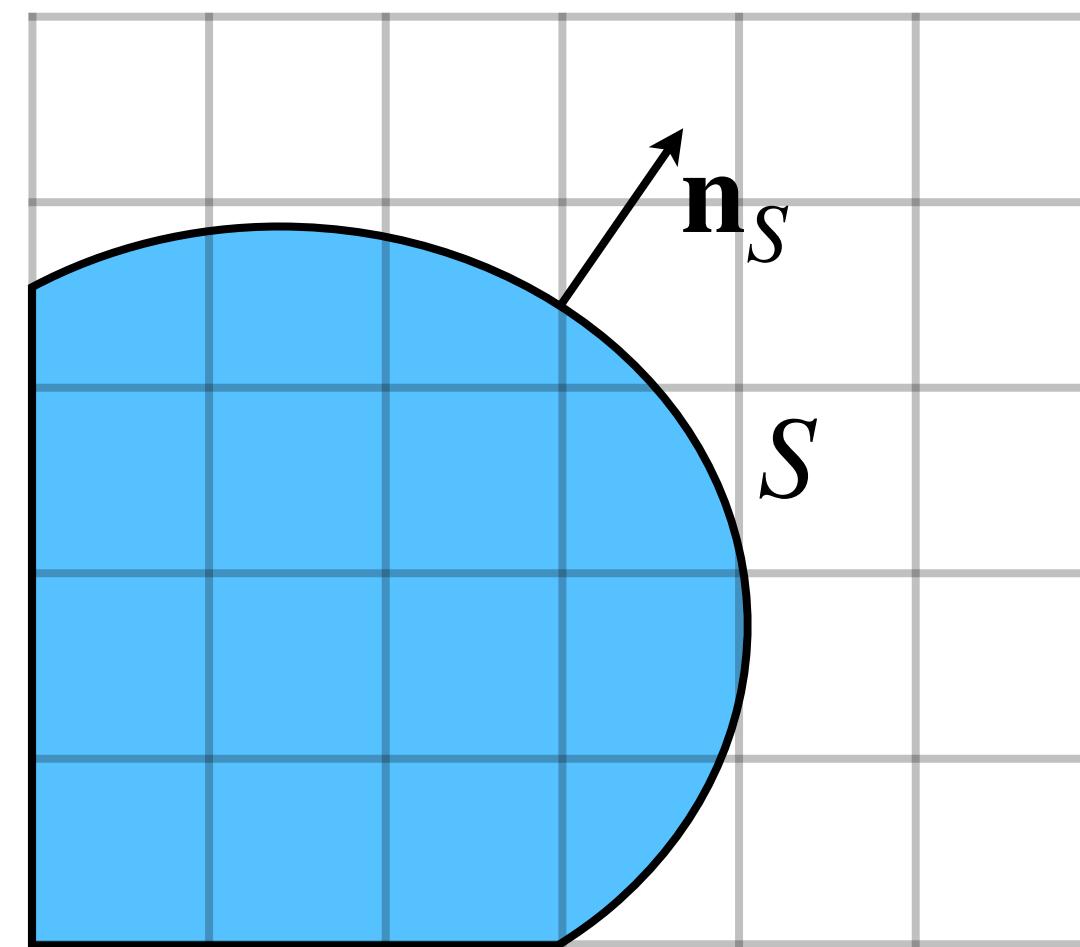


- Discretization

- Finite Volume on Cartesian grid
- SIMPLE for pressure coupling [Patankar 1979]
- VOF advection with reconstruction [Aulisa 2007]
- Linear solvers from Hypre [Falgout 2002]

# Surface tension

- Calculation of surface tension  $\mathbf{f}_\sigma = \sigma \kappa \mathbf{n}_S \delta_S$  relies on interface curvature  $\kappa = \nabla_S \cdot \mathbf{n}_S$
- Existing methods show poor accuracy at low resolution
  - gradients of volume fraction [Brackbill 1992]
  - level-set [Sussman 1998]
  - height functions [Cummins 2005]
  - generalized height functions [Popinet 2009]  
with parabolic fit to mixed heights

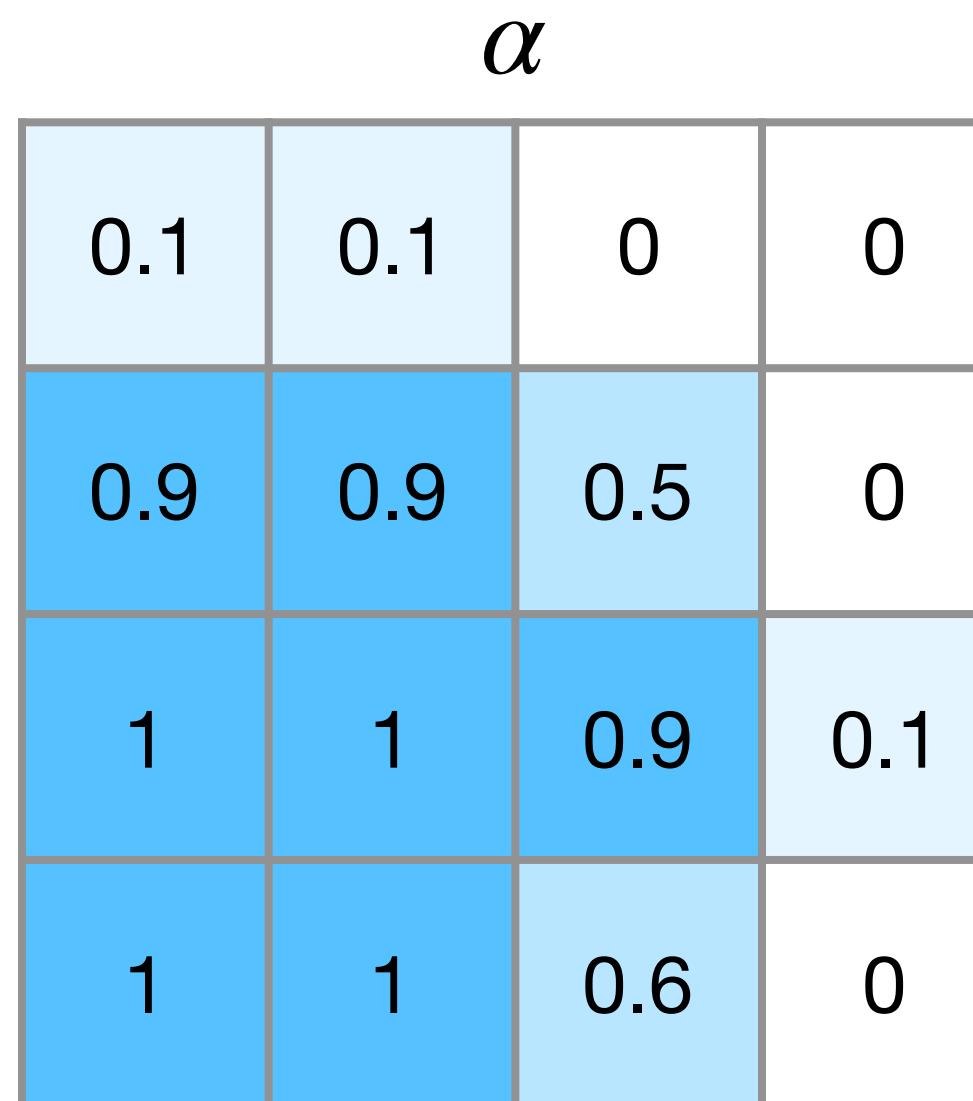


0	0	0	0	0
0	0	0	0.9	1
0	0.5	0.7	1	1
0.5	1	1	1	1

# Piecewise linear interface

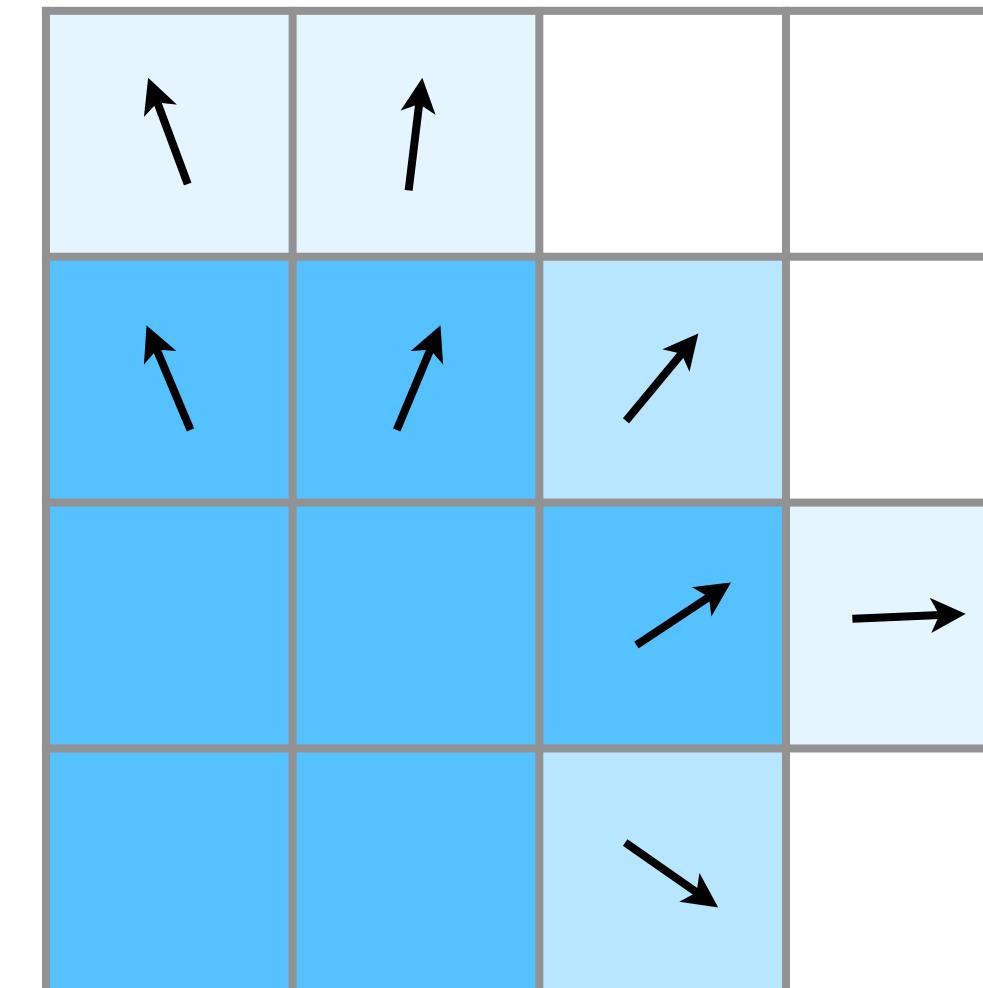
Line segments (2D) or polygons (3D) from volume fractions [Aulisa 2007]

- Volume fraction field

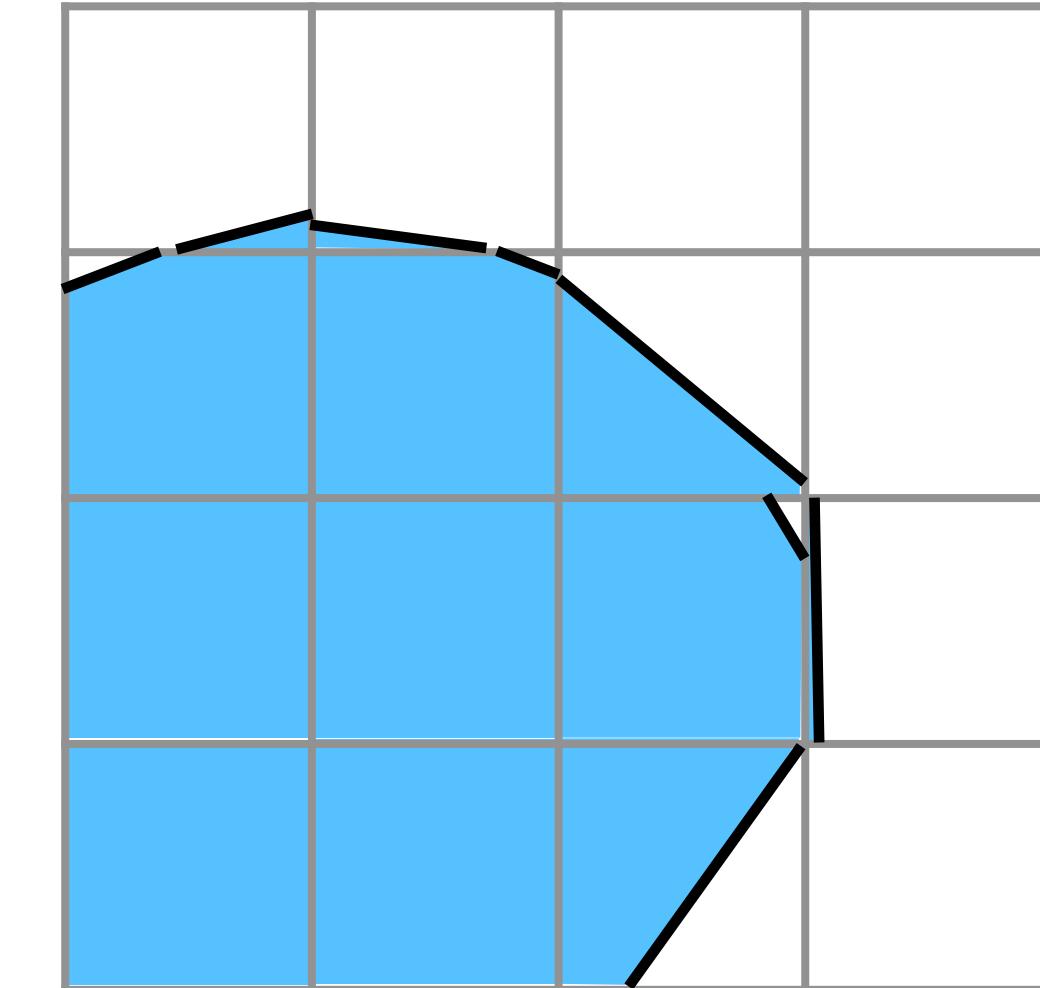


- Normals as gradients

$$\mathbf{n} = -\nabla\alpha$$

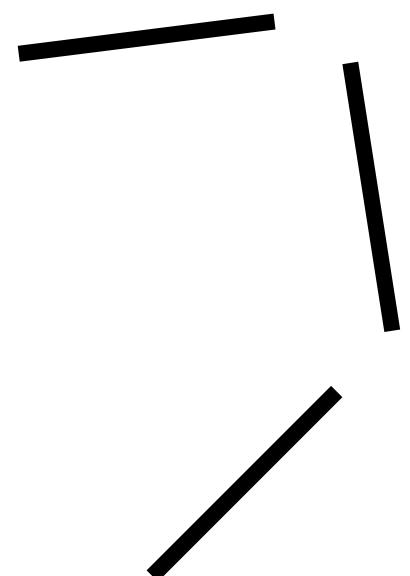


- Lines cutting the cells at given volume fraction

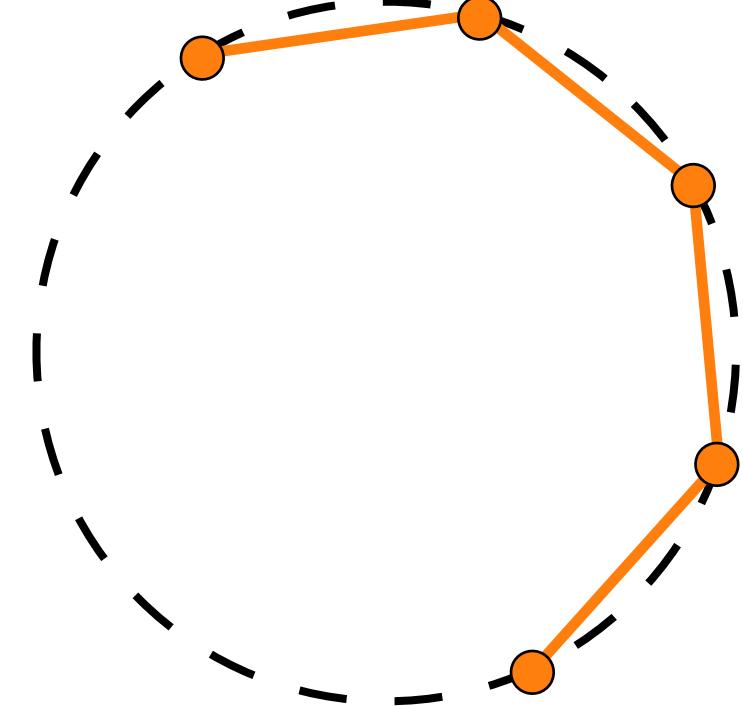


# Proposed method

Estimation of curvature from line segments using particles



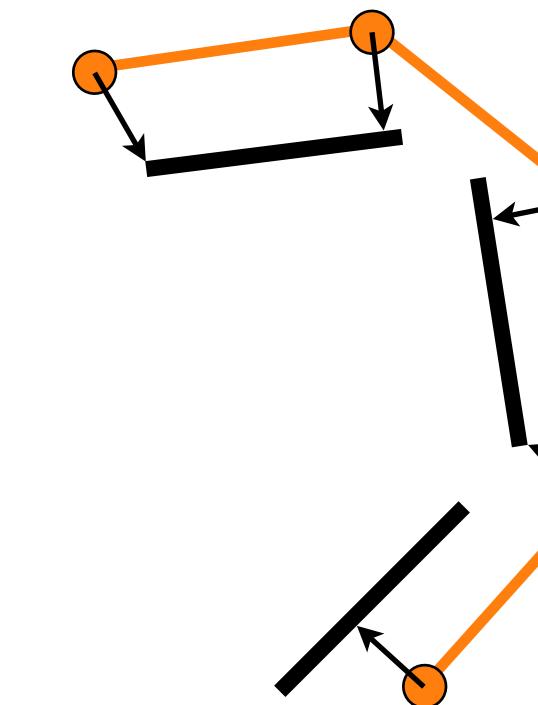
1. Line segments



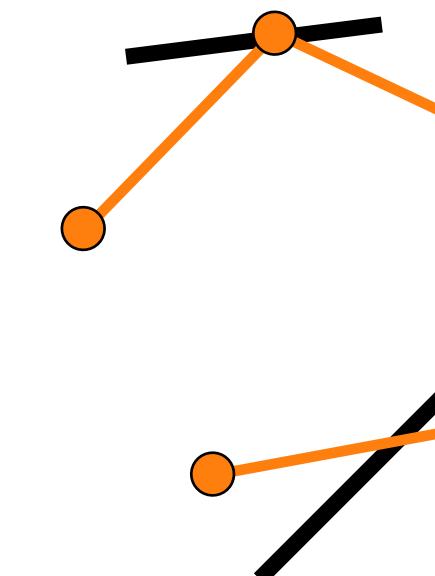
2. Constrained particles

- fixed distance
- uniform angle

⇒ particles belong to a circle



3. Attraction forces



4. Curvature from  
equilibrium positions

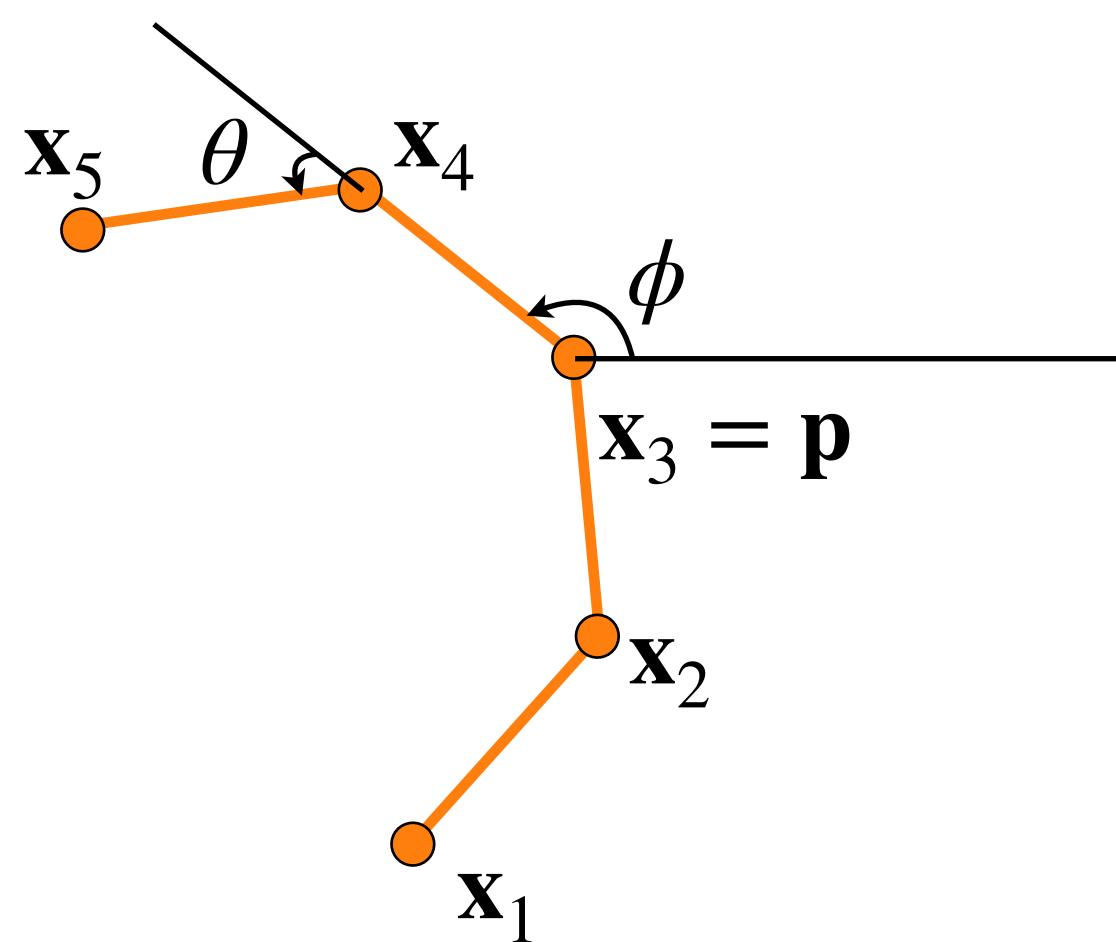
# Proposed method

## Evolution of constrained particles

- Constraints are satisfied by parametrization

$$\mathbf{x}_i = \mathbf{x}_i(\mathbf{p}, \phi, \theta) \quad i = 1, \dots, 5$$

$\mathbf{p}$  position of central particle  
 $\phi$  orientation angle  
 $\theta$  bending angle



- Force  $\mathbf{f}_i$  attracts  $\mathbf{x}_i$  to nearest point on the interface
- Each step applies corrections from projected forces

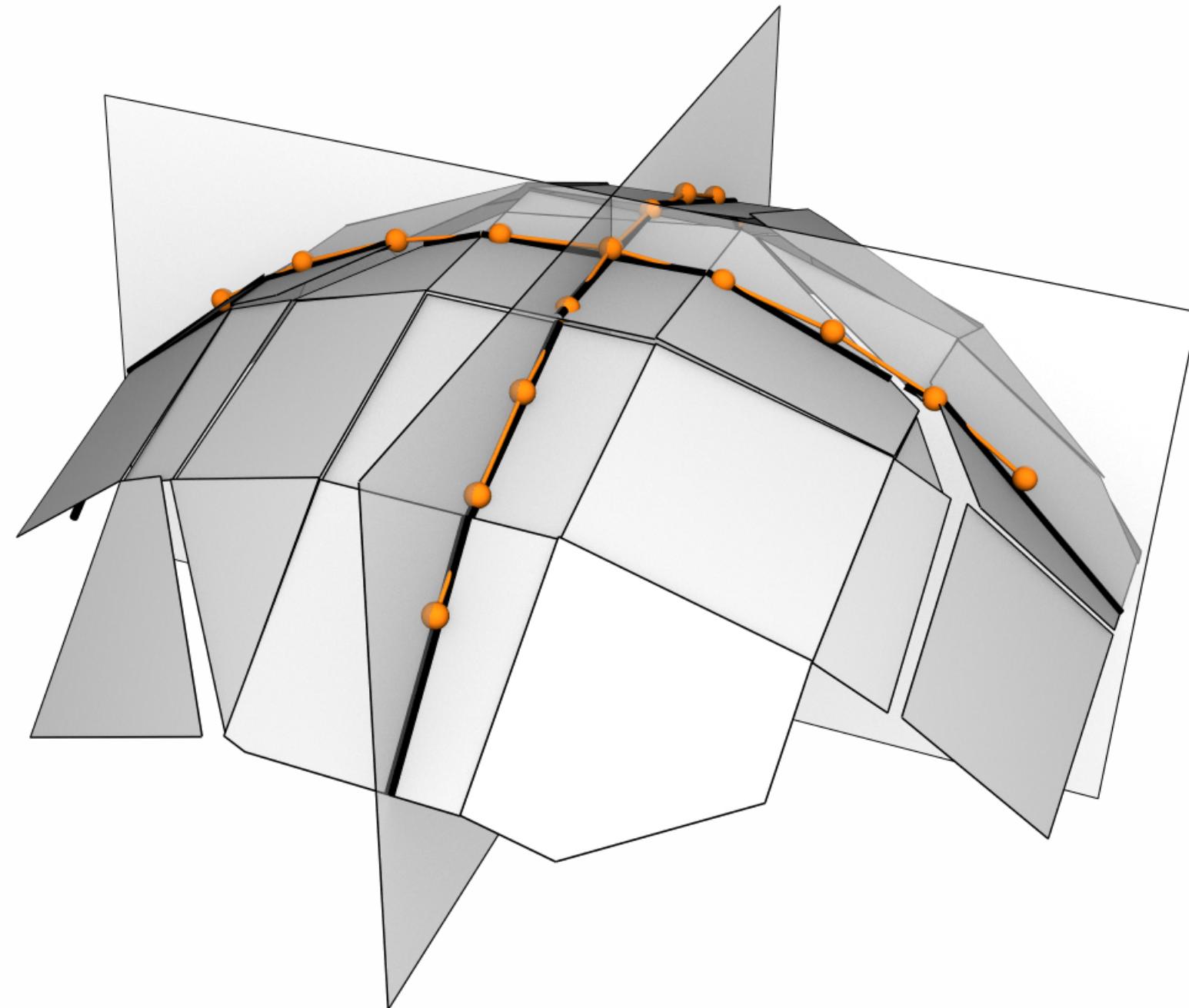
$$\Delta\phi = \sum_i \mathbf{f}_i \cdot \frac{\partial \mathbf{x}_i}{\partial \phi} / \sum_i \frac{\partial \mathbf{x}_i}{\partial \phi} \cdot \frac{\partial \mathbf{x}_i}{\partial \phi}$$

(similar for  $\mathbf{p}$  and  $\theta$ )

# Proposed method

## Mean curvature in 3D

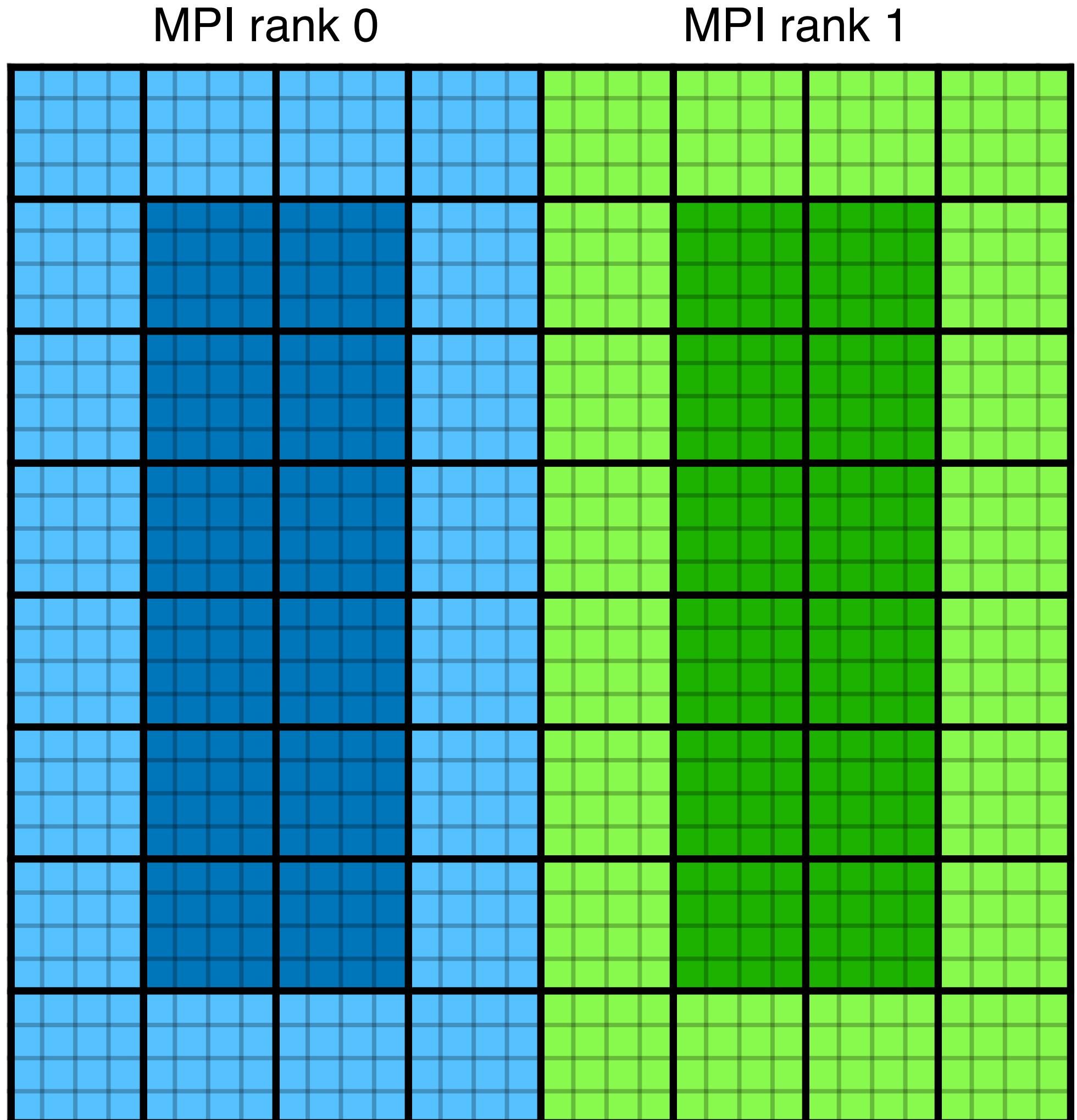
- Interface consists of polygons
- Mean curvature is the average over cross-sections normal to the interface
- Cross-section consists of line segments  
⇒ problem reduced to 2D



# Implementation

# Blockwise processing

- Each rank splits its subdomain to cubic blocks
  - cache utilization
  - compute-transfer overlap:  
communication while computing inner blocks
- Used in Cubism-MPCF [Rossinelli 2013, Wermelinger 2018]  
Multiphase compressible flows  
Gordon Bell prize 2013 for high throughput computation
- Drawback: lack of modularity



# Example

- Block processor executes kernels on blocks and calls MPI to exchange ghost cells
- Adding communication requires changing the block processor

- Algorithm 1: one stage

$$\mathbf{u}^{n+1} = \text{AD}(\mathbf{u}^n)$$

```
block processor
for (Block b : bb) {
    AD(b);
}
Comm();
```

- Algorithm 2: two stages

$$\mathbf{u}^{n+1/2} = \text{A}(\mathbf{u}^n)$$

$$\mathbf{u}^{n+1} = \text{D}(\mathbf{u}^{n+1/2})$$

```
block processor
for (Block b : bb) {
    A(b);
}
Comm();
for (Block b : bb) {
    D(b);
}
Comm();
```

MPI rank 0	MPI rank 1
AD	AD
AD	AD

communication

MPI rank 0	MPI rank 1
A	A
A	A

communication

D	D
D	D

communication

Kernels:

A advection

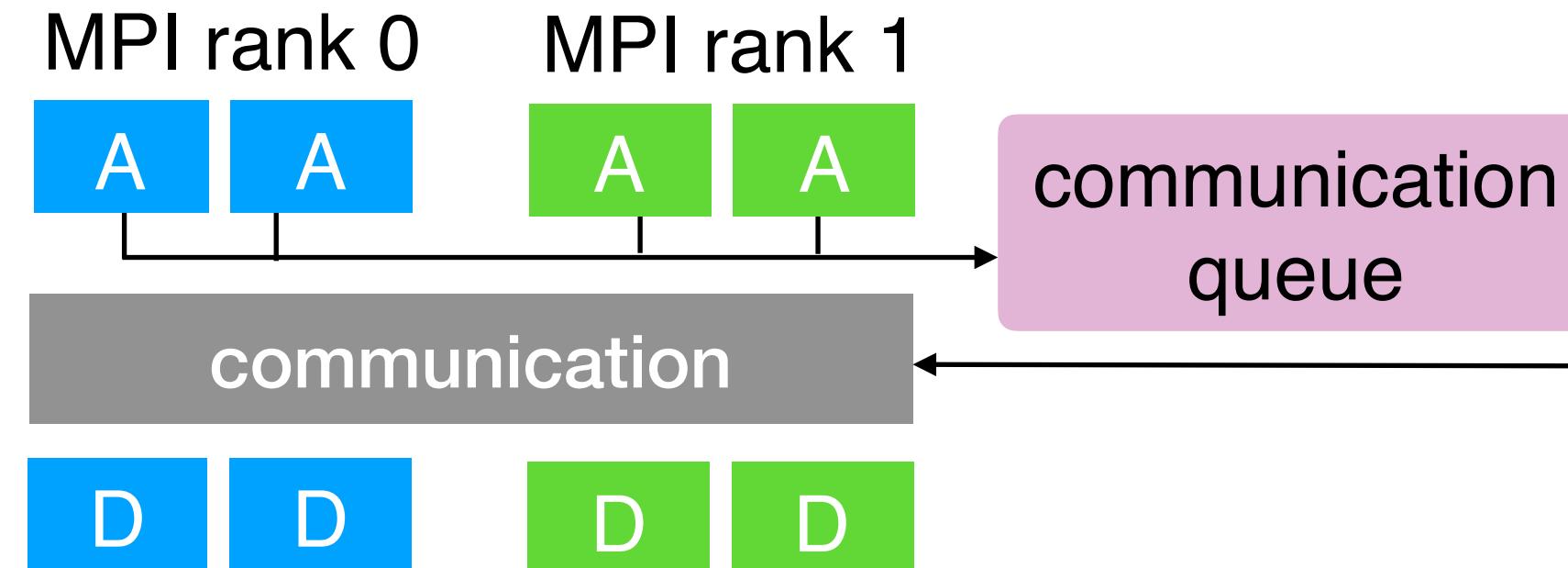
D diffusion

AD advection+diffusion

# Coroutines

kernel

```
void AD(Block b, Queue q) {
    A(b);
    q.RequestComm(b);
    yield;
    D(b);
}
```



block processor

```
Queue q;
while (!q.Done()) {
    for (Block b : bb) {
        AD(b, q);
    }
    Comm(q);
}
```

emulation of coroutines in C++

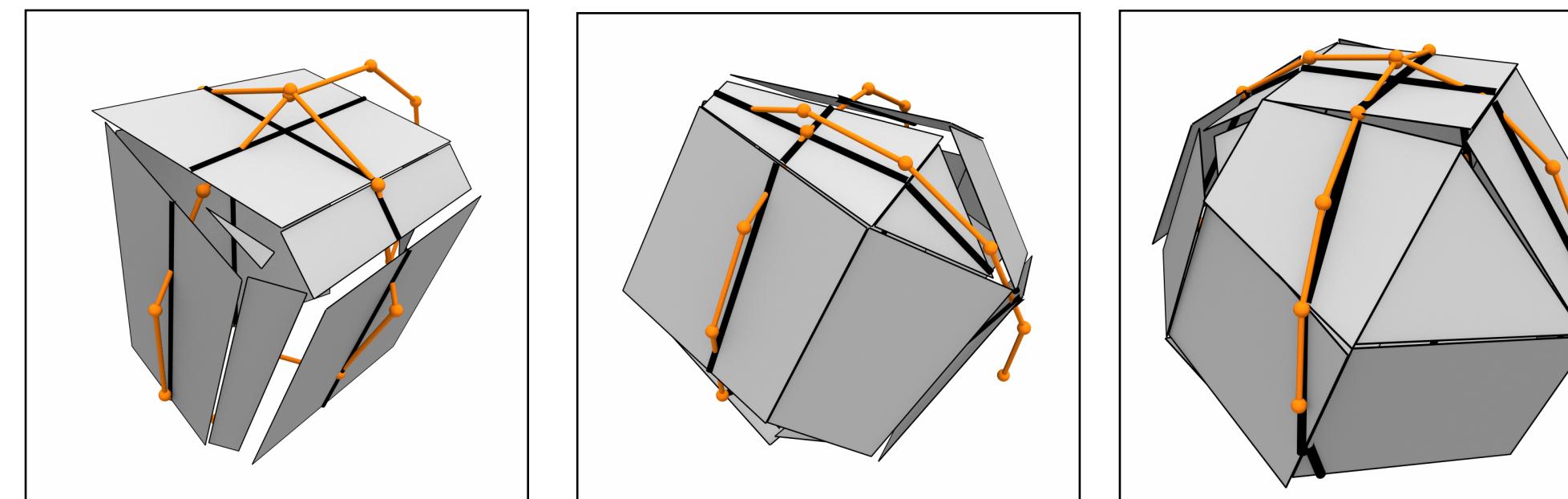
```
void AD(Block b, Queue q) {
    Stages s(b);
    if (s()) {
        A(b);
        q.RequestComm(b);
    }
    if (s()) {
        D(b);
    }
}
```

- Kernels can request communication and suspend
- Universal block processor executes the requests
- Enables modularity
  - kernels control communication
  - allows nested calls

# Test cases

# Curvature of a sphere

- Error in curvature relative to exact value
- Comparison to Basilisk  
generalized height-function method [Popinet 2009] [basilisk.fr]
- Present method
  - more accurate at resolutions below 12 cells
  - error below 10% even with one cell per radius



cells per radius: 0.59

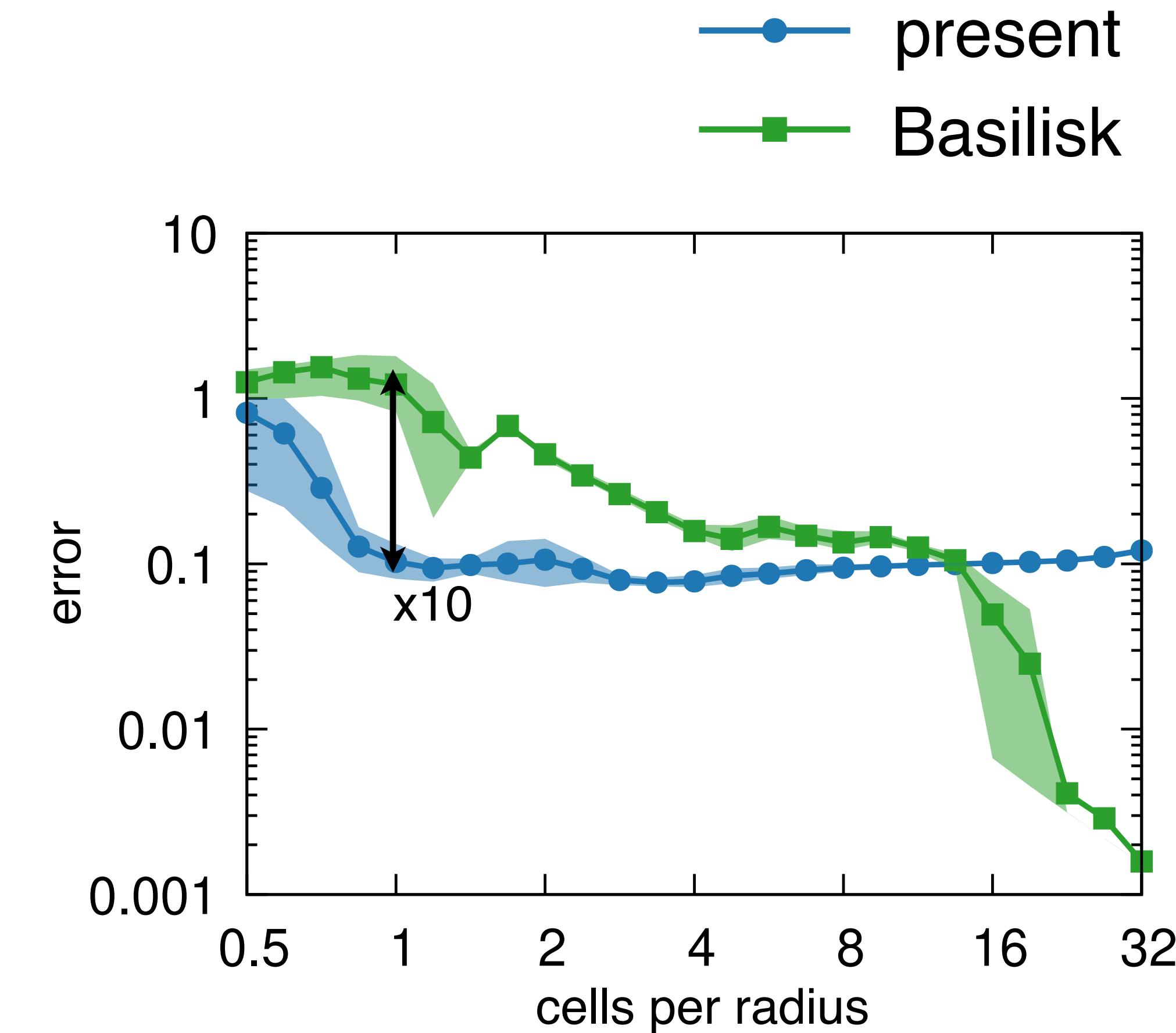
error: 0.42

cells per radius: 0.84

error: 0.08

cells per radius: 1.19

error: 0.09



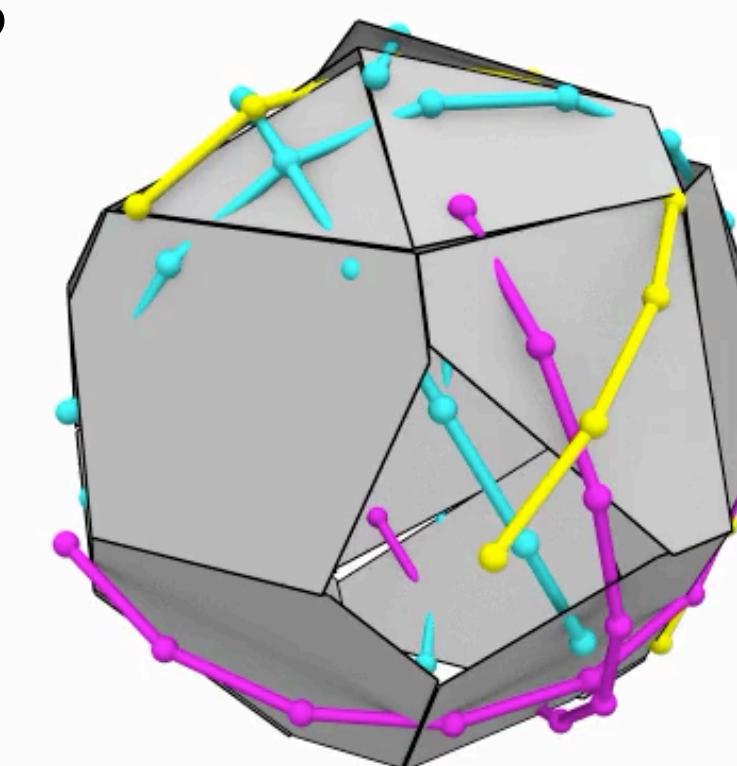
# Translating droplet

- Uniform initial velocity  $\mathbf{u}_0$

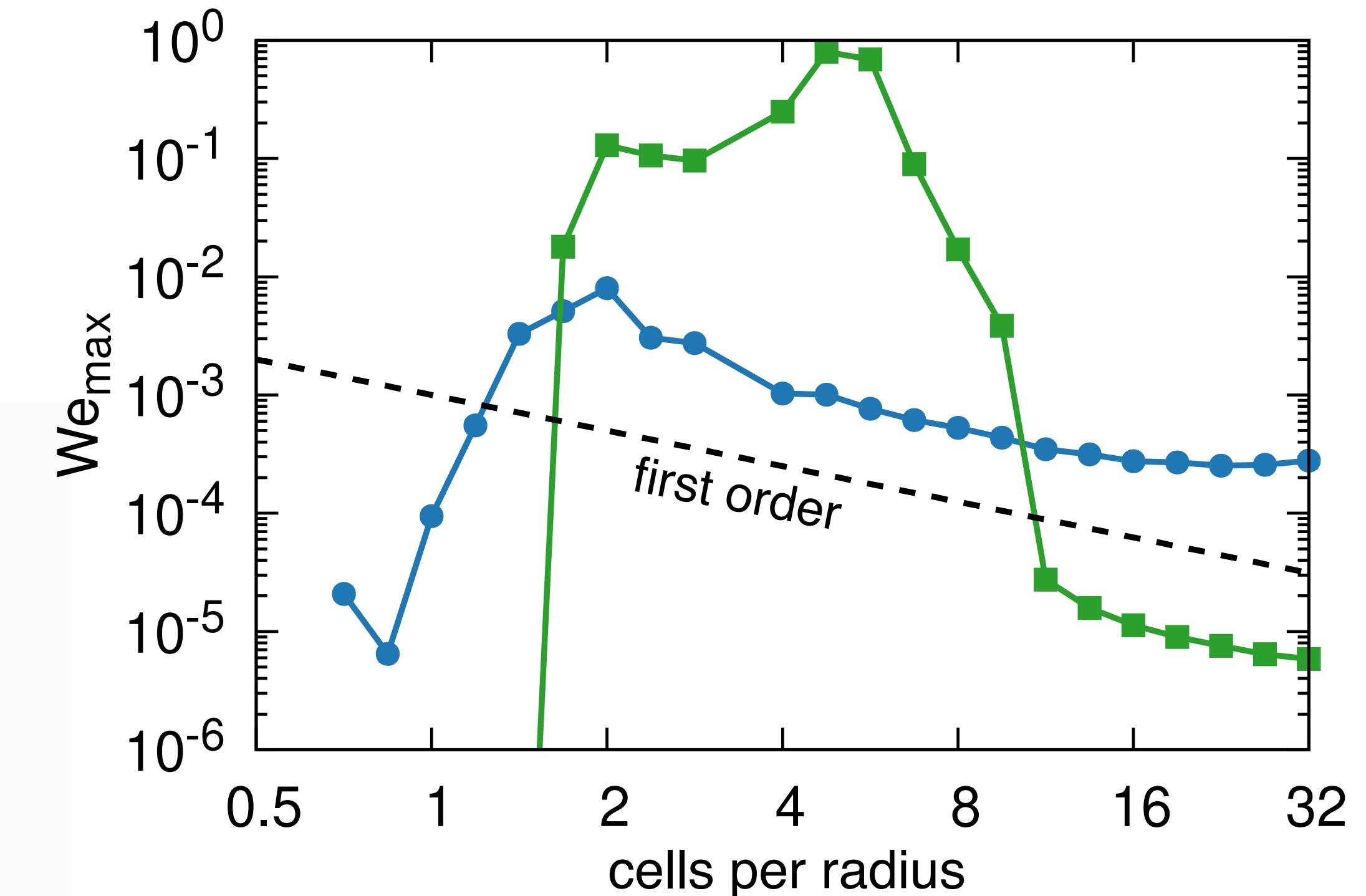
- Spurious flow created by inaccuracies in curvature

- Present method

- lower magnitude of spurious flow at resolutions below 10 cells
- small droplets act as tracers



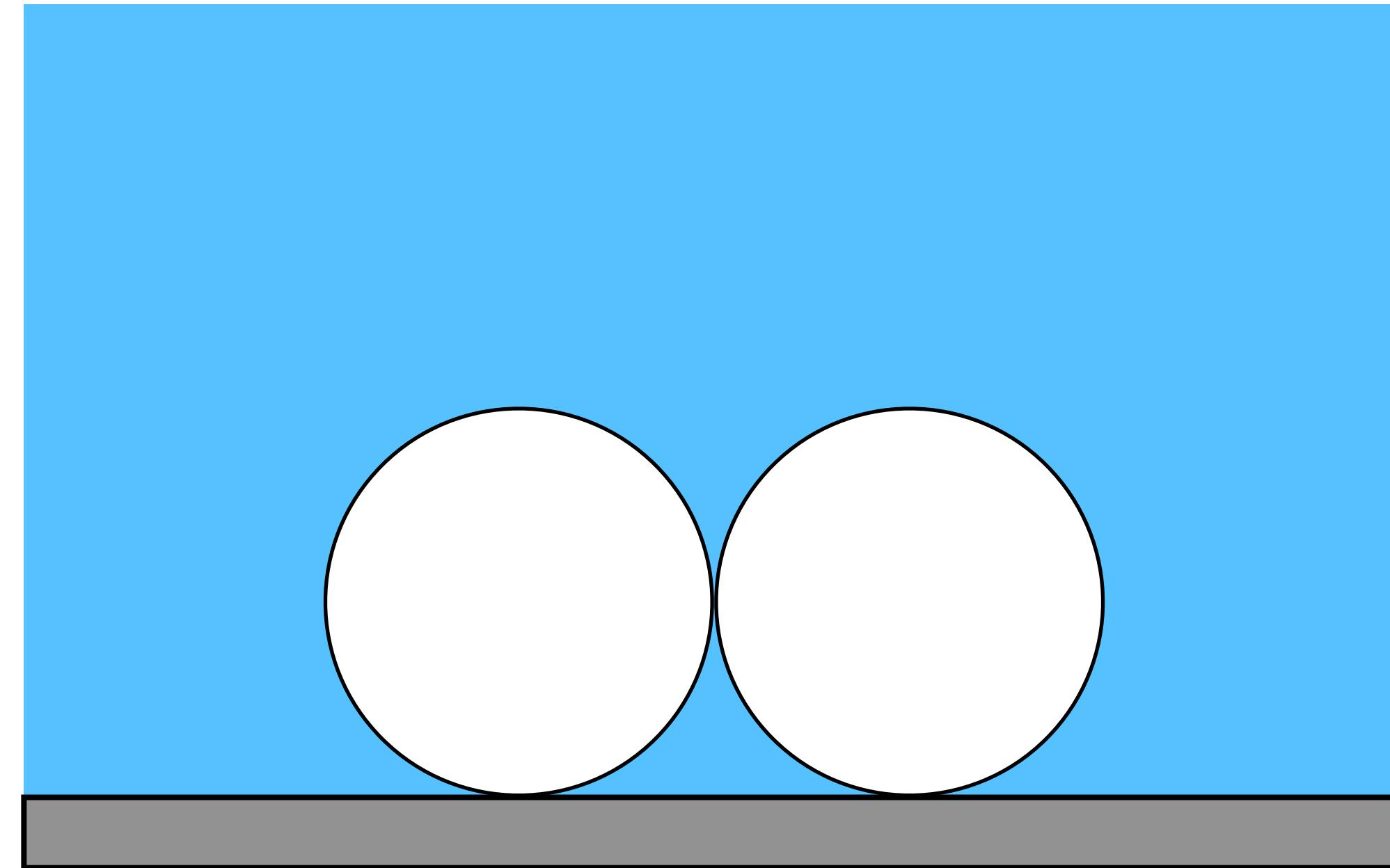
$$\text{We}_{\max} = \frac{2\rho R}{\sigma} \max |\mathbf{u} - \mathbf{u}_0|^2 \quad \text{magnitude of spurious flow in terms of Weber number}$$



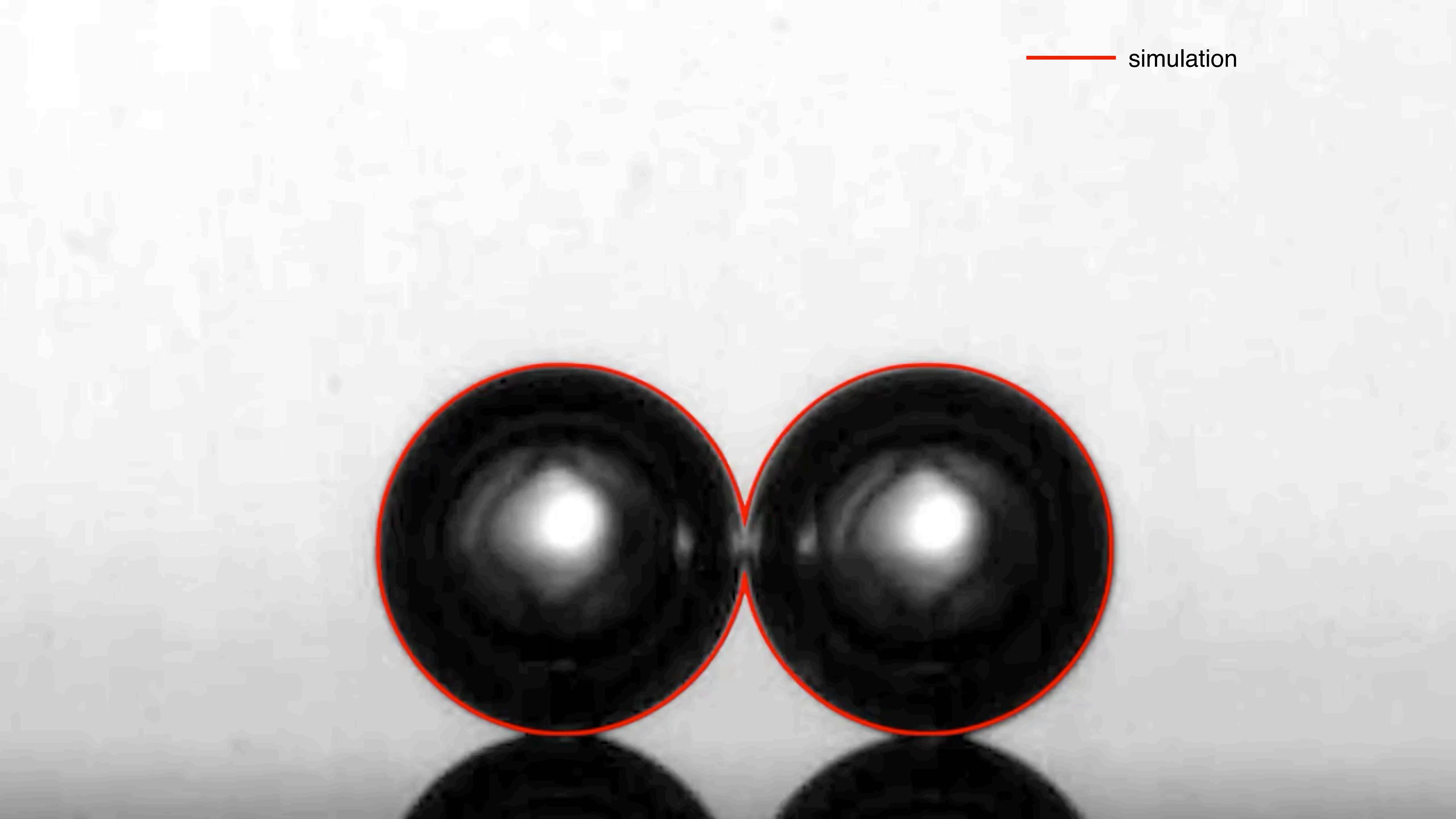
# Applications

# Coalescence of bubbles

- Experiment on near-wall coalescence
- Bubbles grow due to diffusion of dissolved gas
- Simulations reproduce the experiment



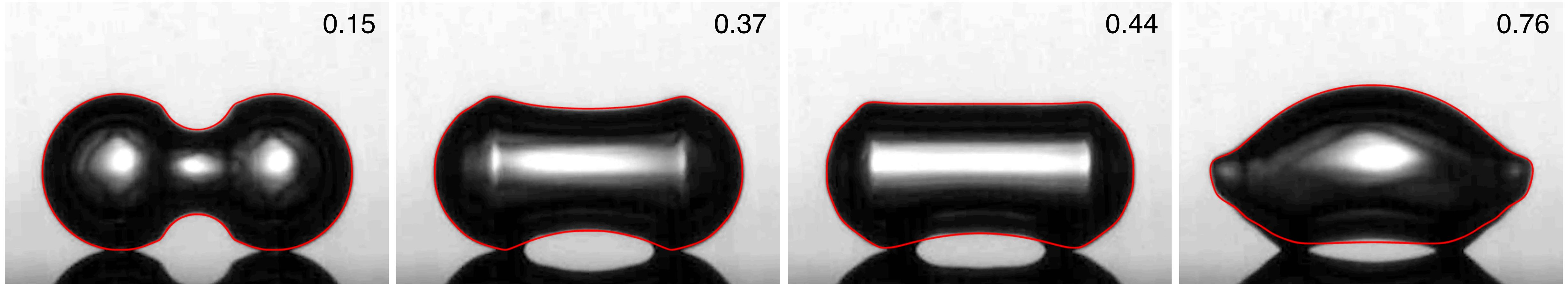
Soto ÁM, Maddalena T, Fraters A, Van Der Meer D, Lohse D.  
Coalescence of diffusively growing gas bubbles.  
Journal of fluid mechanics. 2018



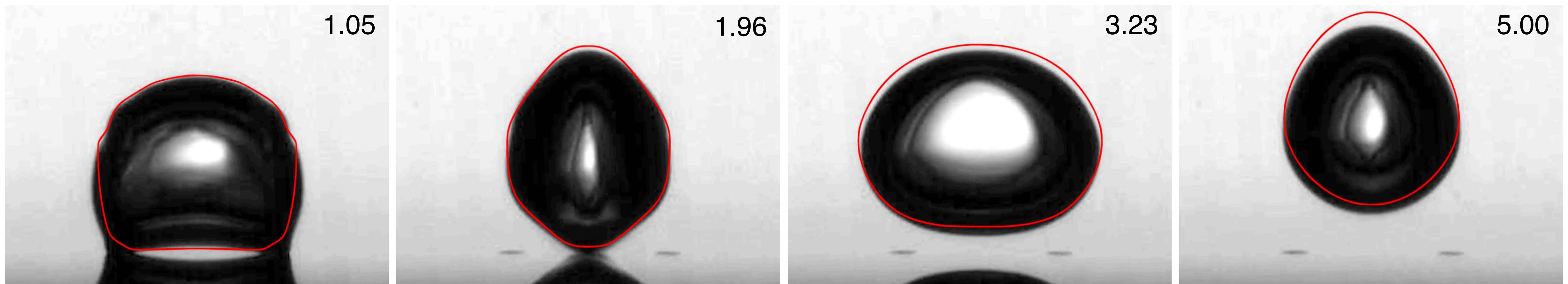
simulation

# Coalescence of bubbles

— simulation



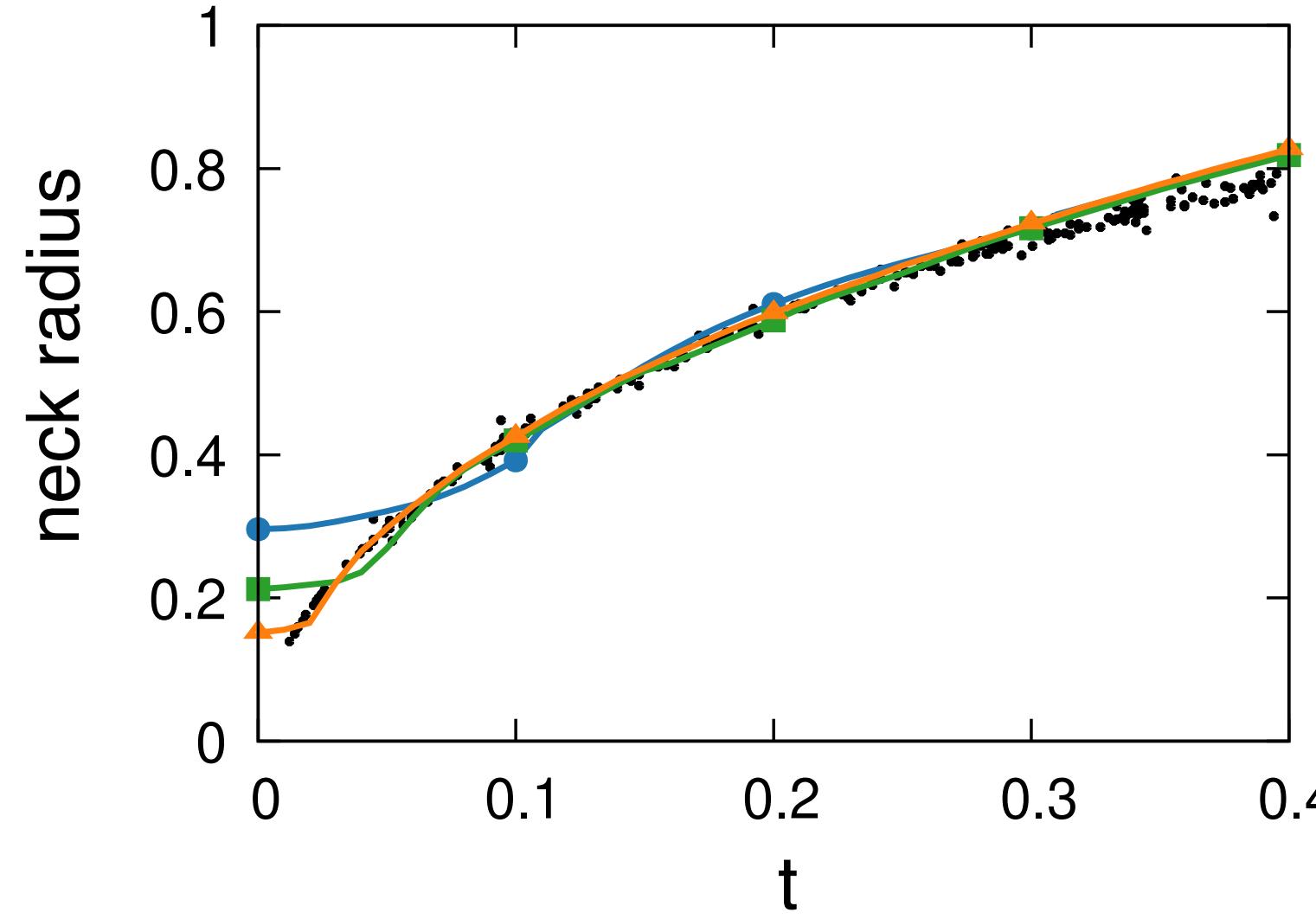
coalescence neck



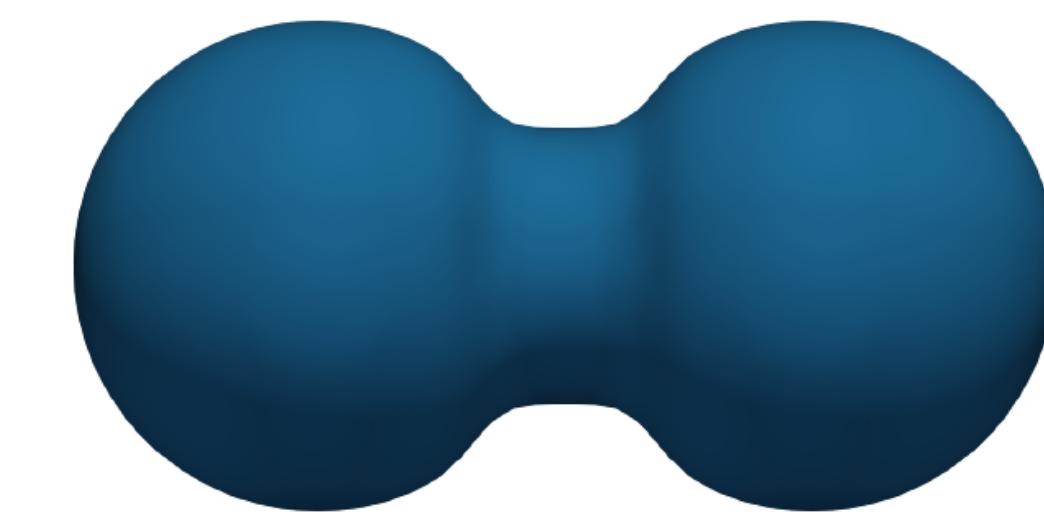
detachment

oscillations

# Coalescence of bubbles

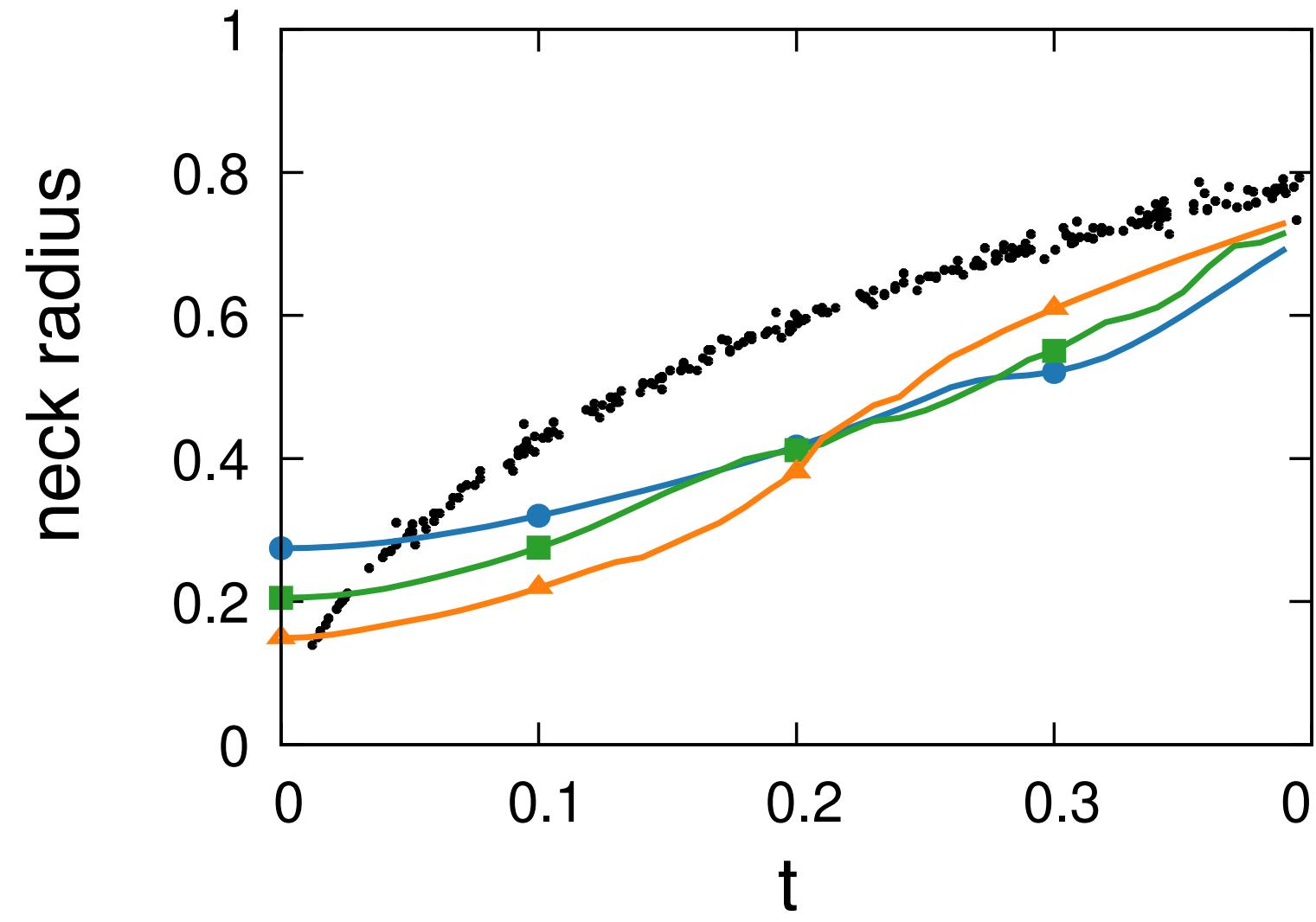


present

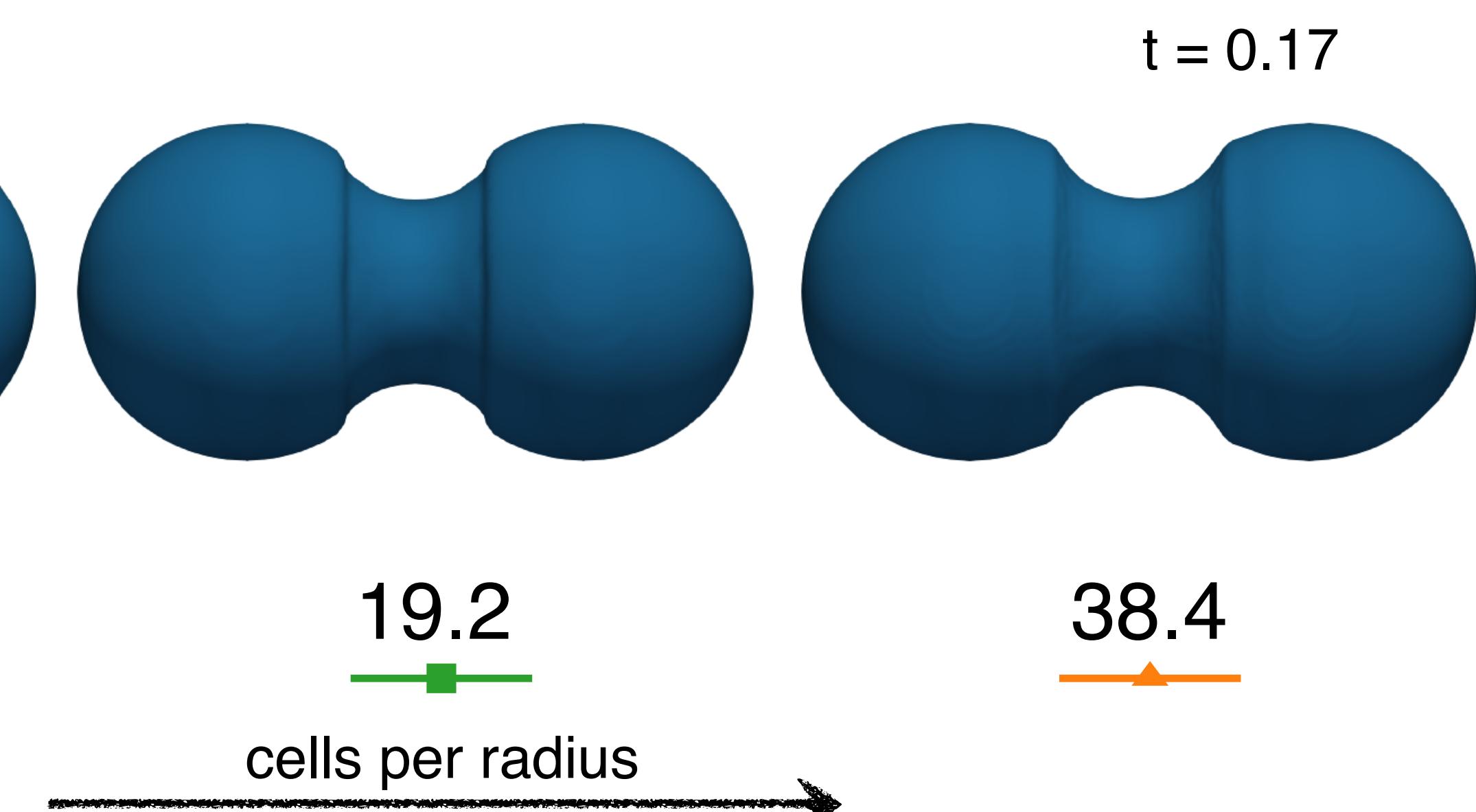


9.6

Basilisk



Basilisk



$t = 0.17$

19.2

38.4

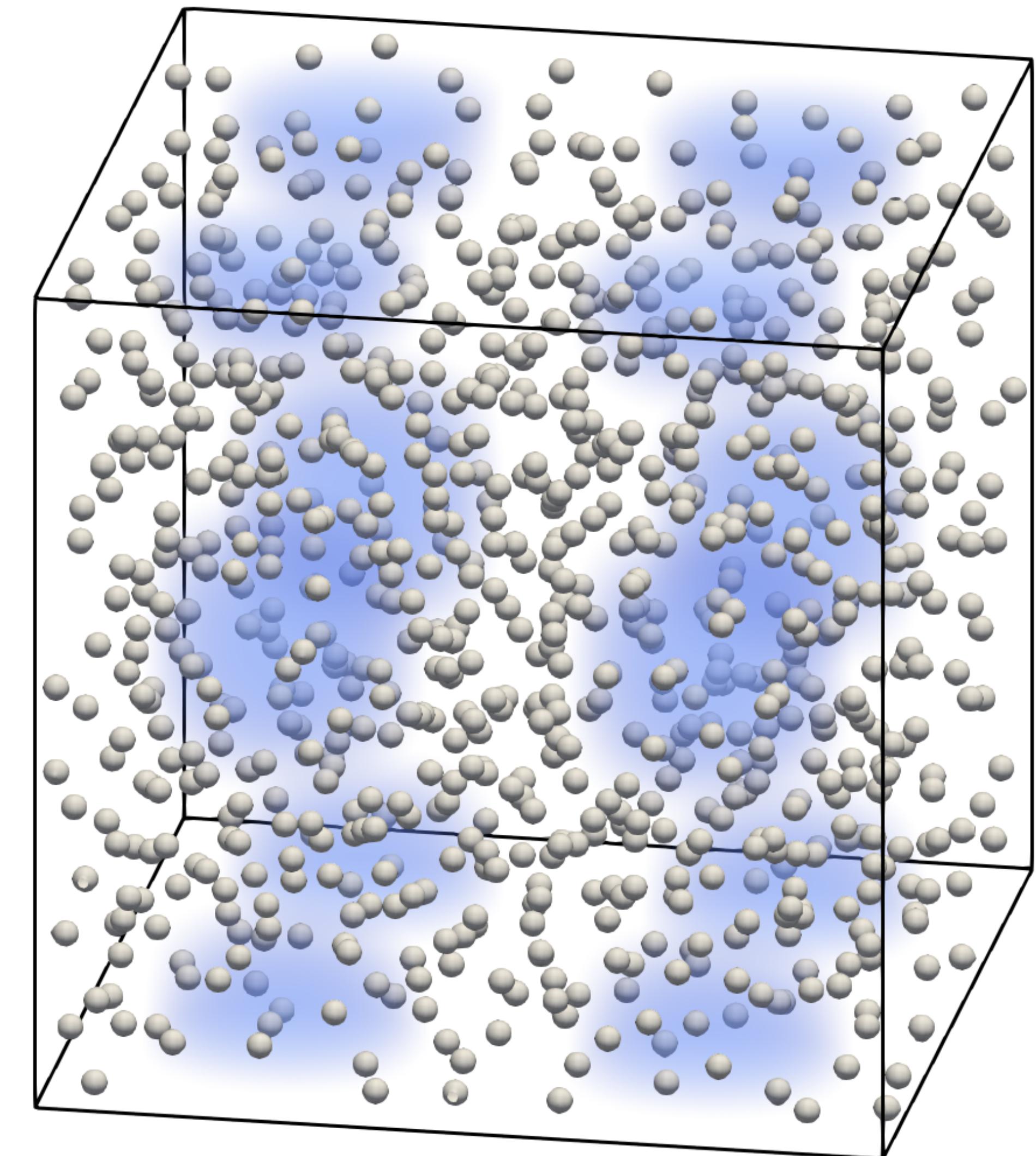
cells per radius

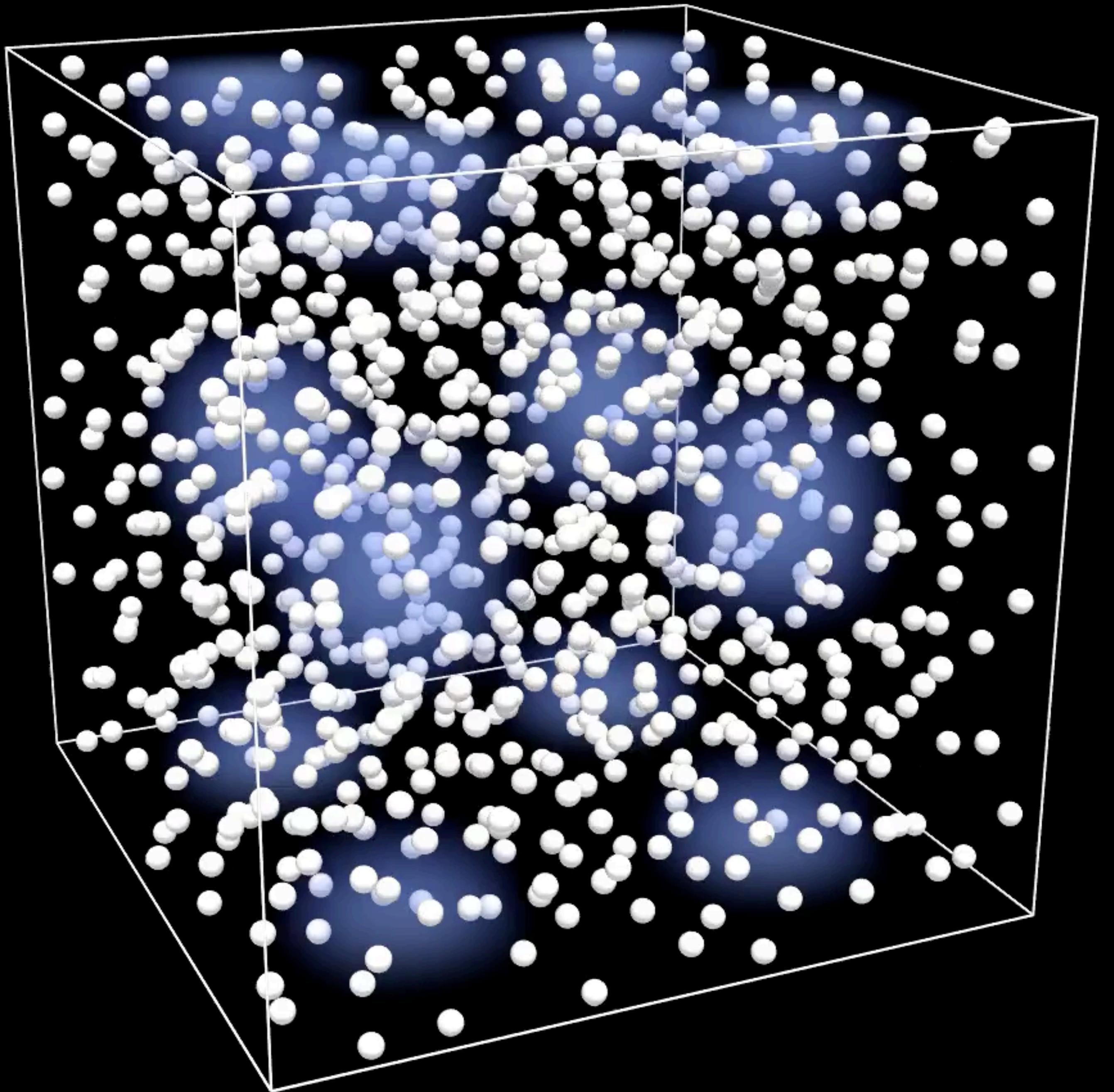
# Taylor-Green vortex with bubbles

- Periodic domain  $[0, 2\pi]^3$
- Initial velocity
 
$$u_x = \sin x \cos y \cos z$$

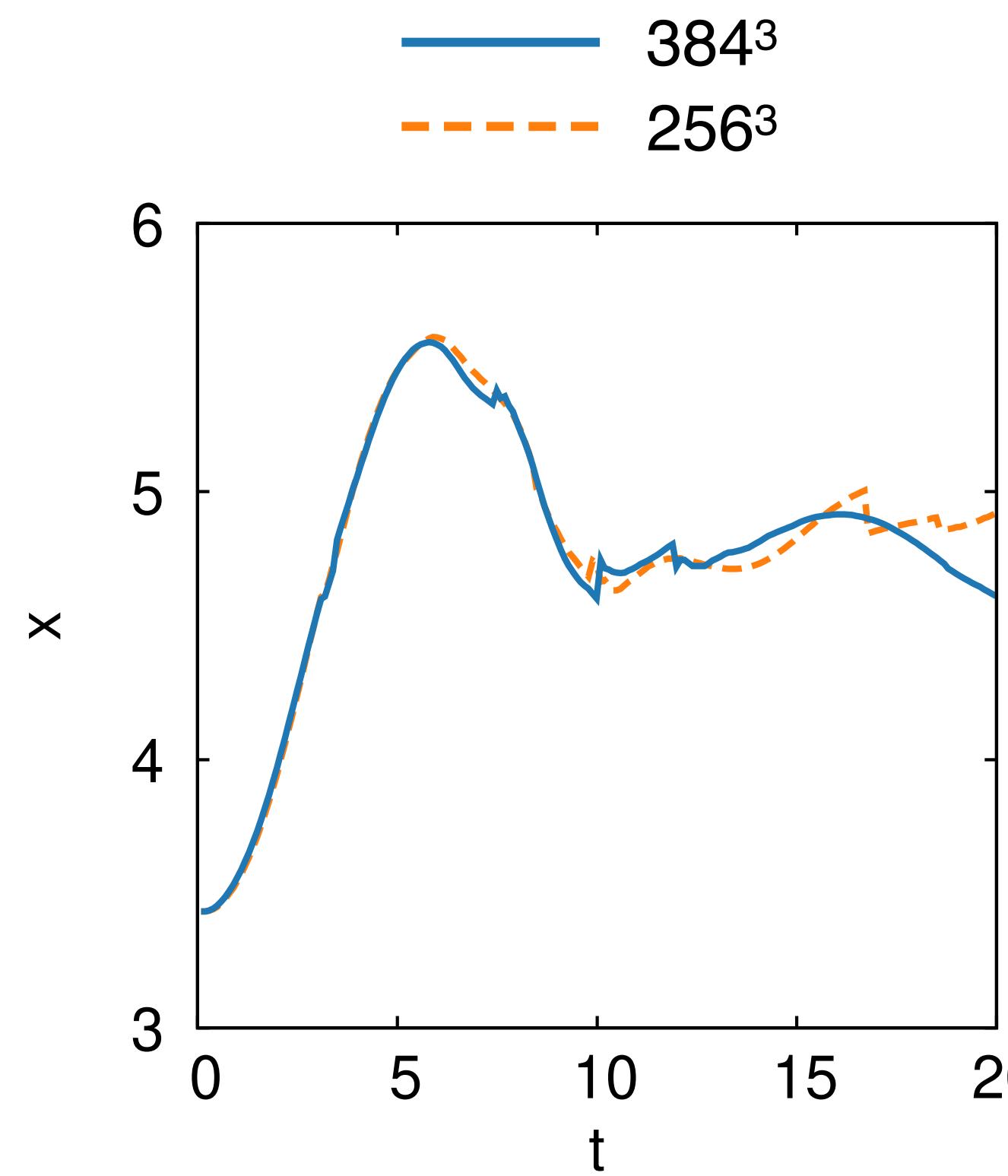
$$u_y = -\cos x \sin y \cos z$$

$$u_z = 0$$
- 890 bubbles, volume fraction 1.4%
- $\text{Re} = \frac{\rho}{\mu} = 1600$        $\text{We} = \frac{2\rho R}{\sigma} = 2$
- Mesh  $256^3$  or  $384^3$

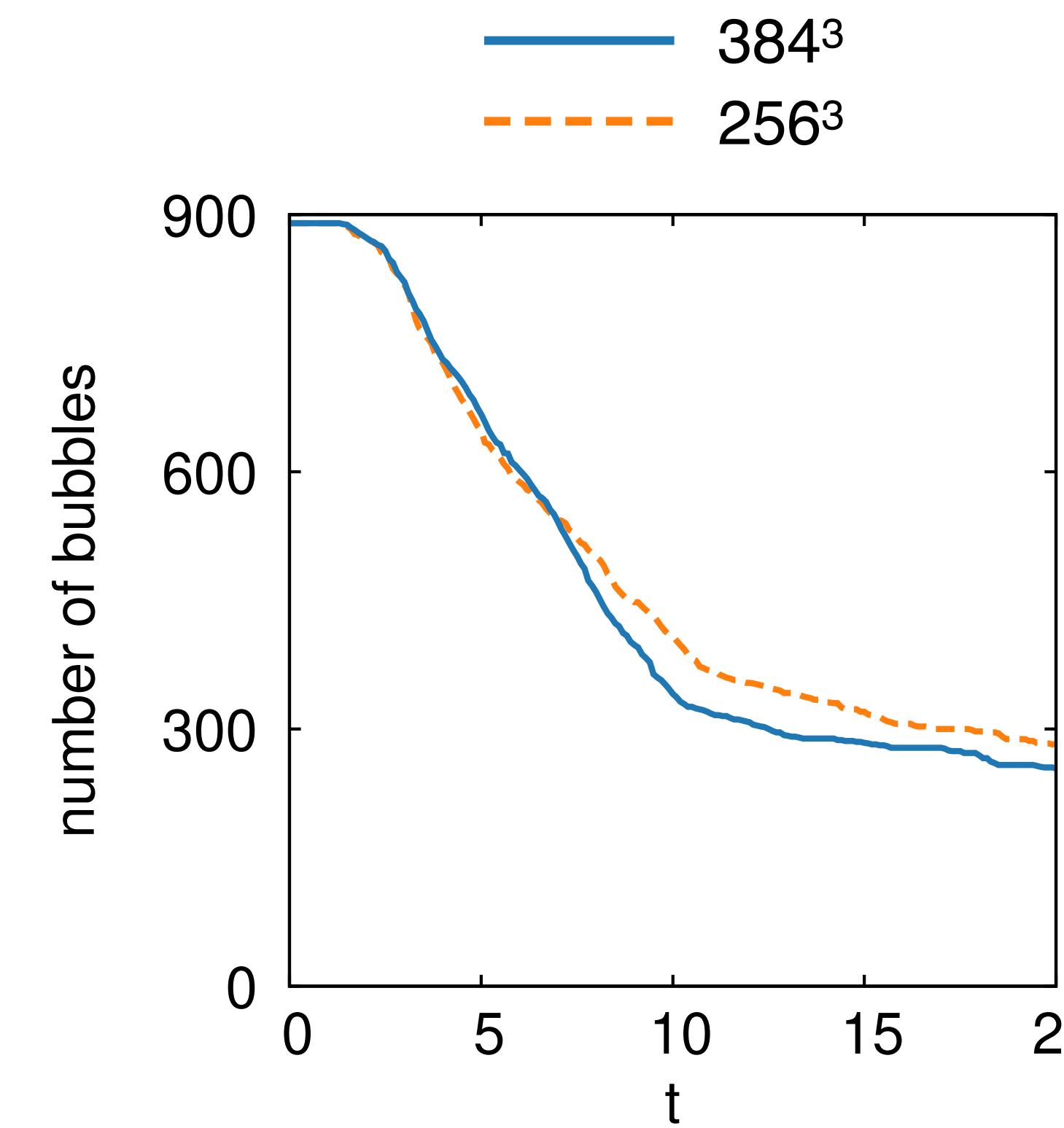




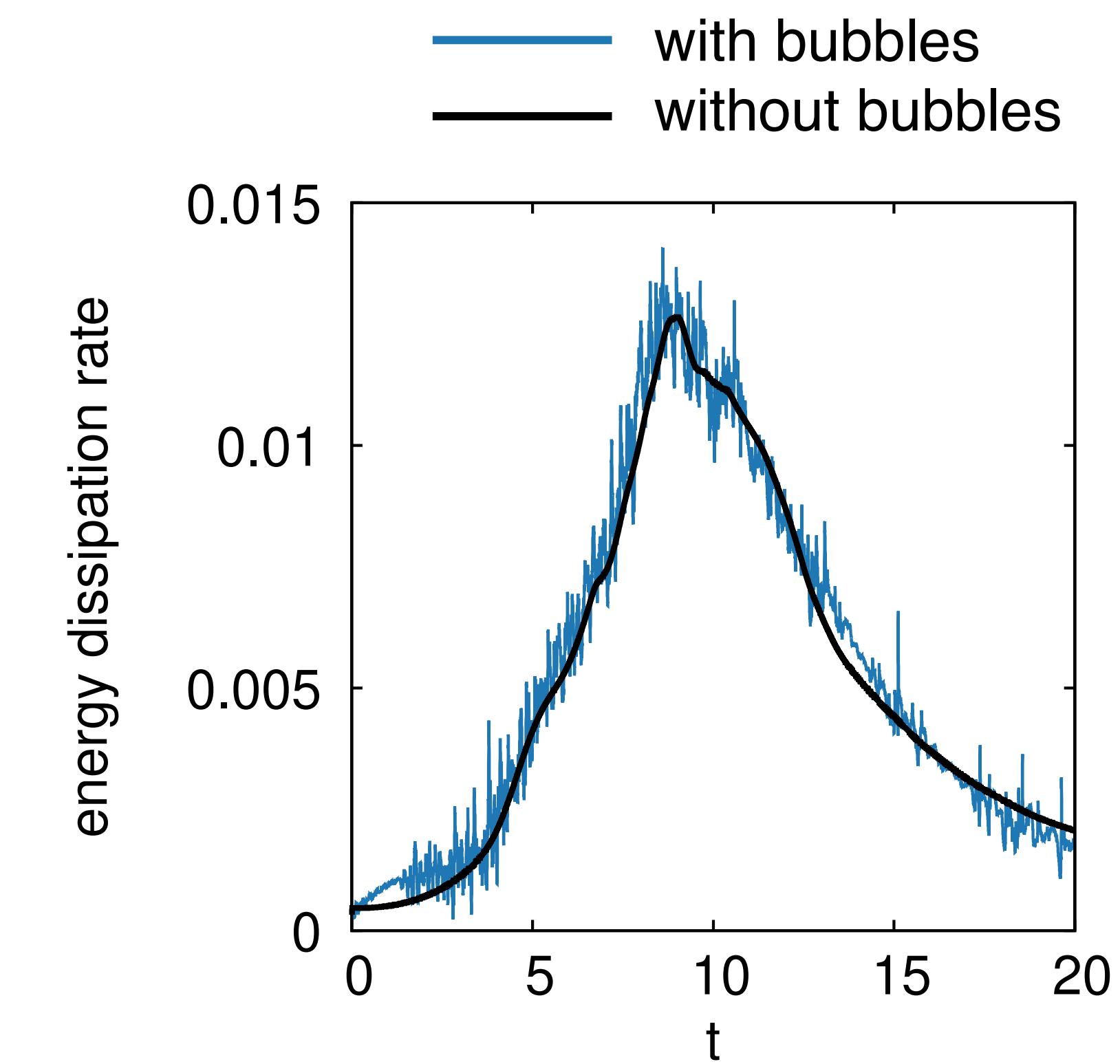
# Taylor-Green vortex with bubbles



trajectory of one bubble,  
no change on finer mesh



number of bubbles reduces  
with time due to coalescence

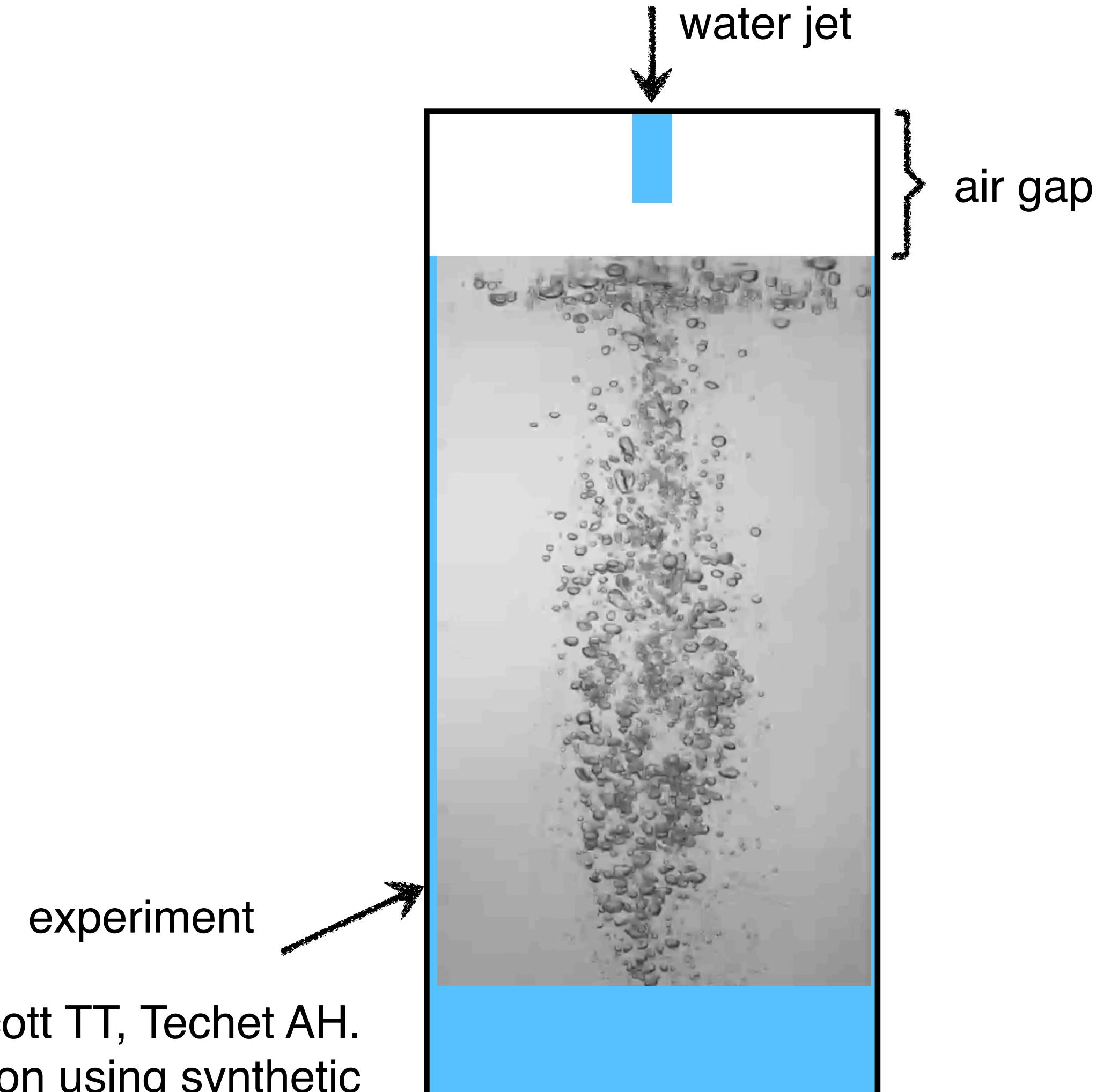


coalescence causes  
fluctuations of dissipation rate

# Plunging jet with air entrainment

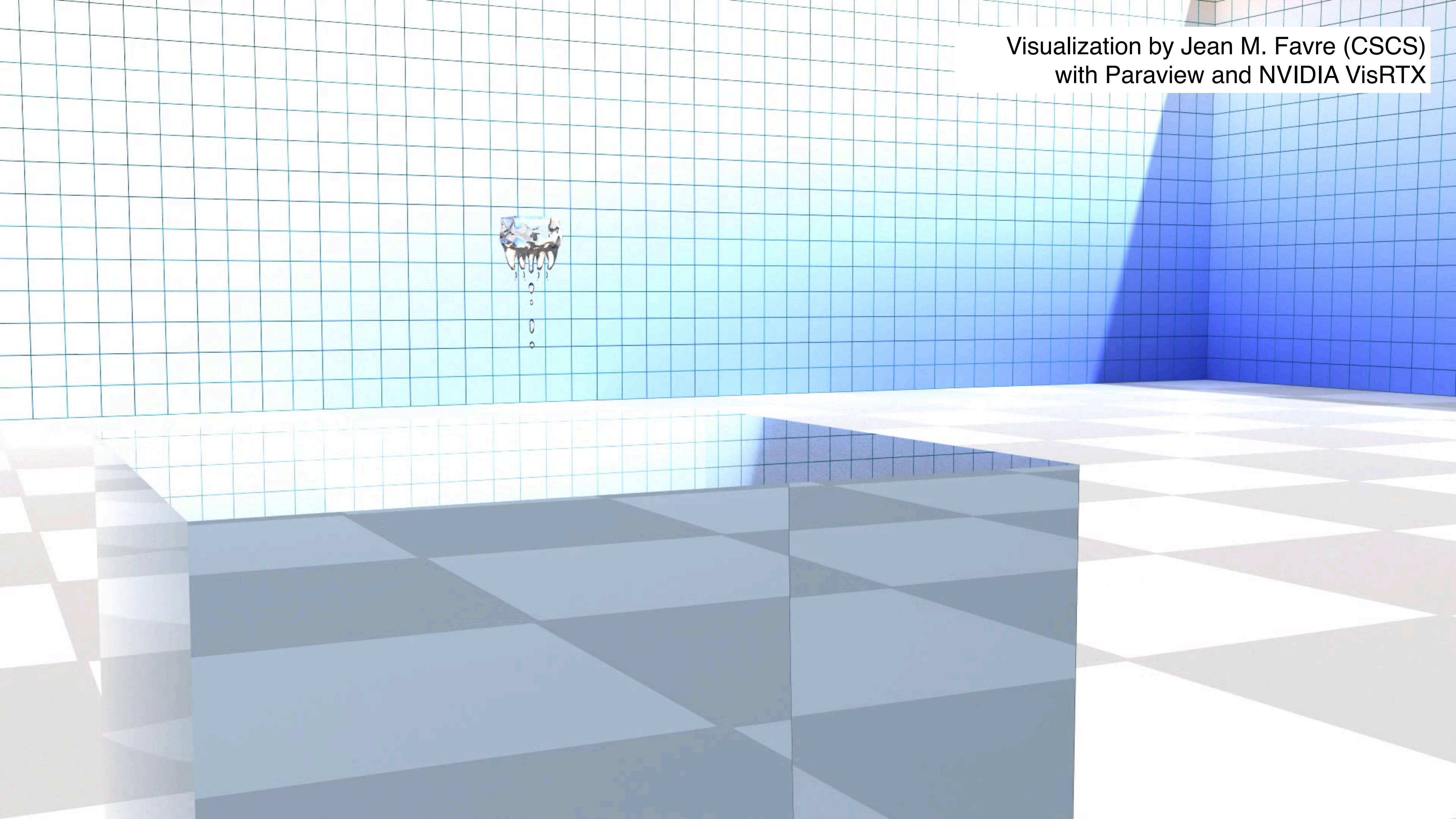
Water jet impacts the free surface

- Box width 10 cm
- Free-slip walls
- Jet diameter 6 mm, velocity 4 m/s
- Mesh 256 x 1024 x 256



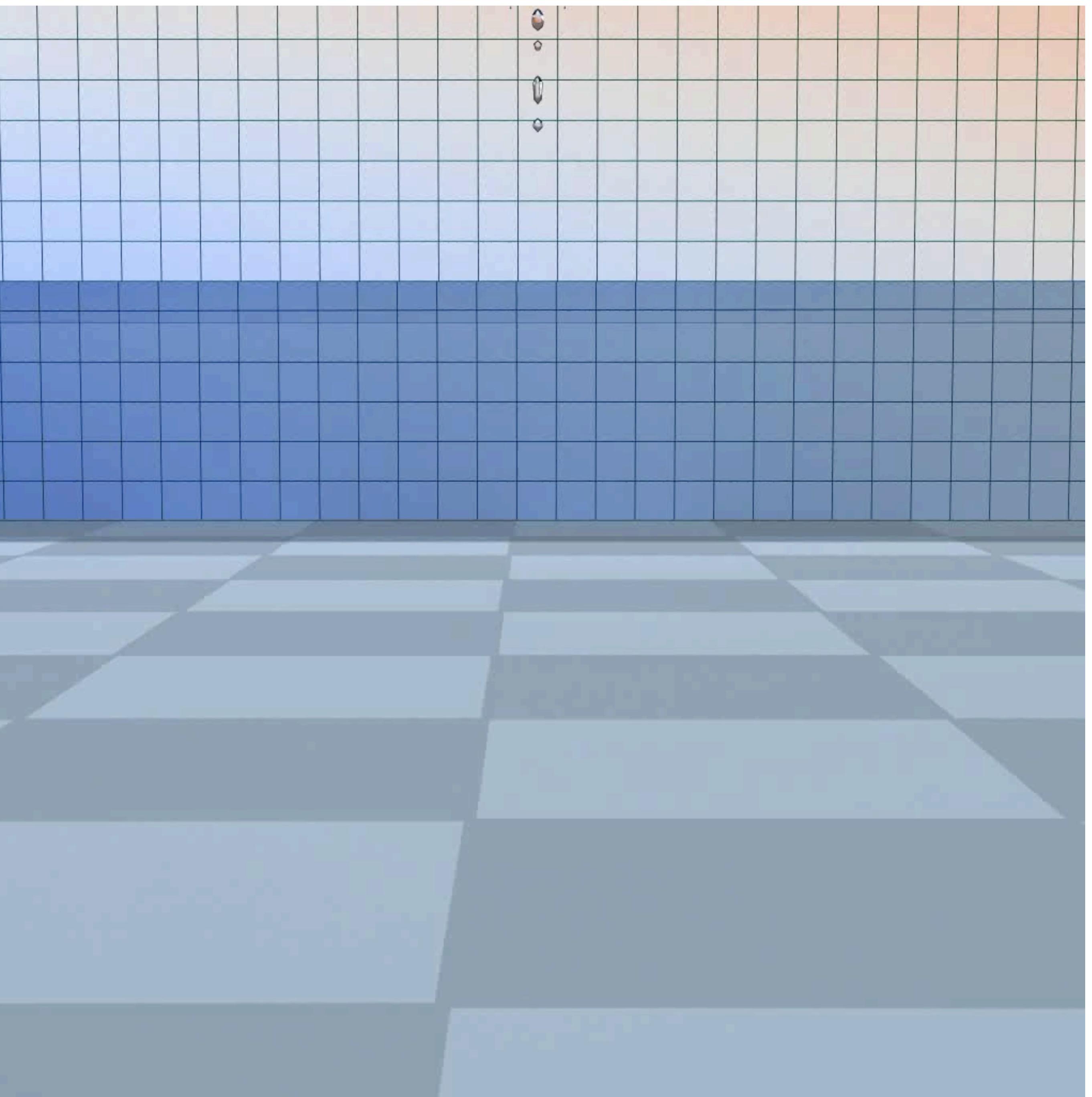
Belden J, Ravela S, Truscott TT, Techet AH.  
Three-dimensional bubble field resolution using synthetic  
aperture imaging: application to a plunging jet.  
Experiments in fluids. 2012

Visualization by Jean M. Favre (CSCS)  
with Paraview and NVIDIA VisRTX



## 1. Liquid jet impact

- large air cavity
- then small bubbles

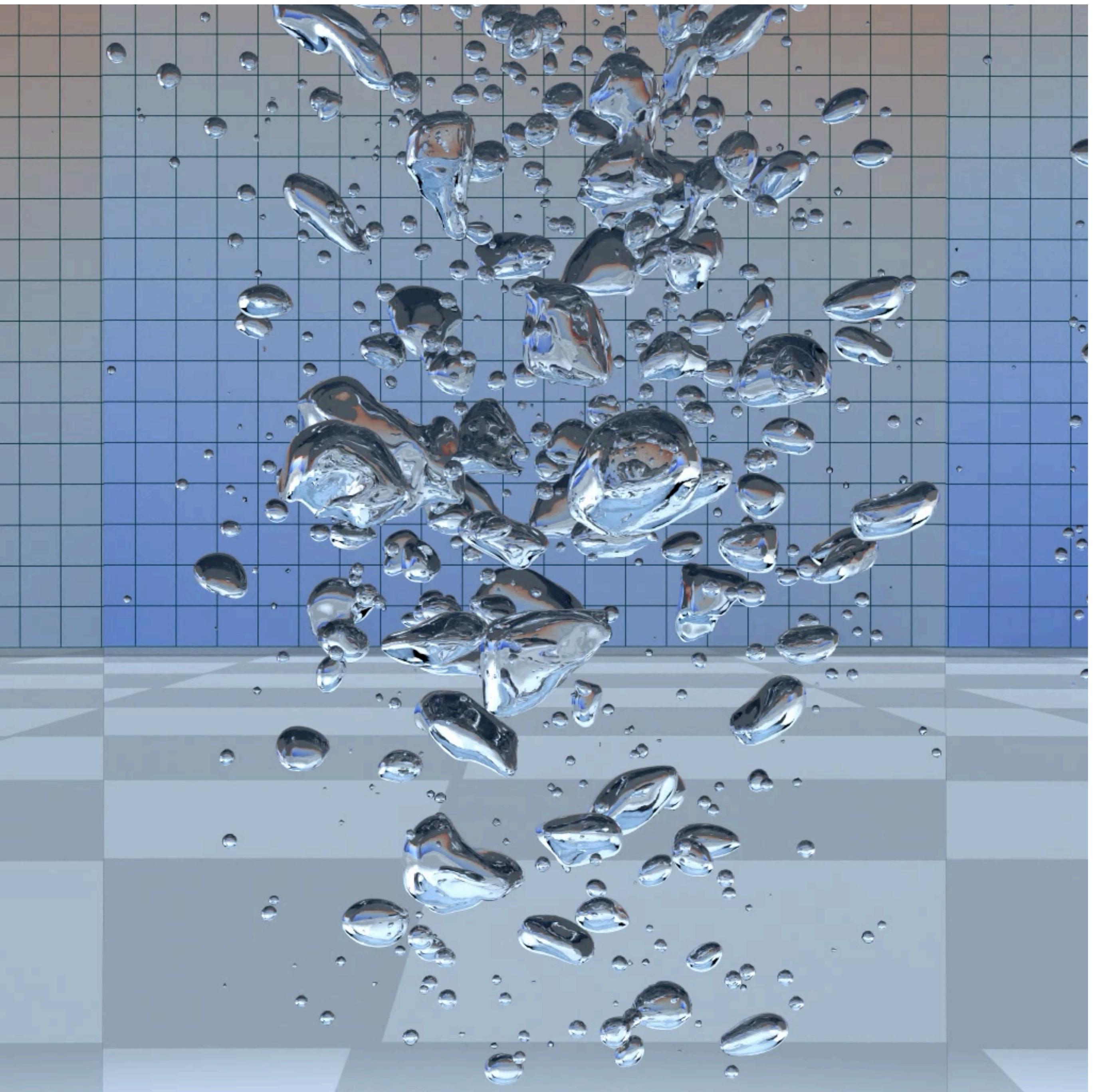


Visualization by Jean M. Favre (CSCS)  
with Paraview and NVIDIA VisRTX

## 2. Stagnation zone

- larger bubbles  
form due to coalescence

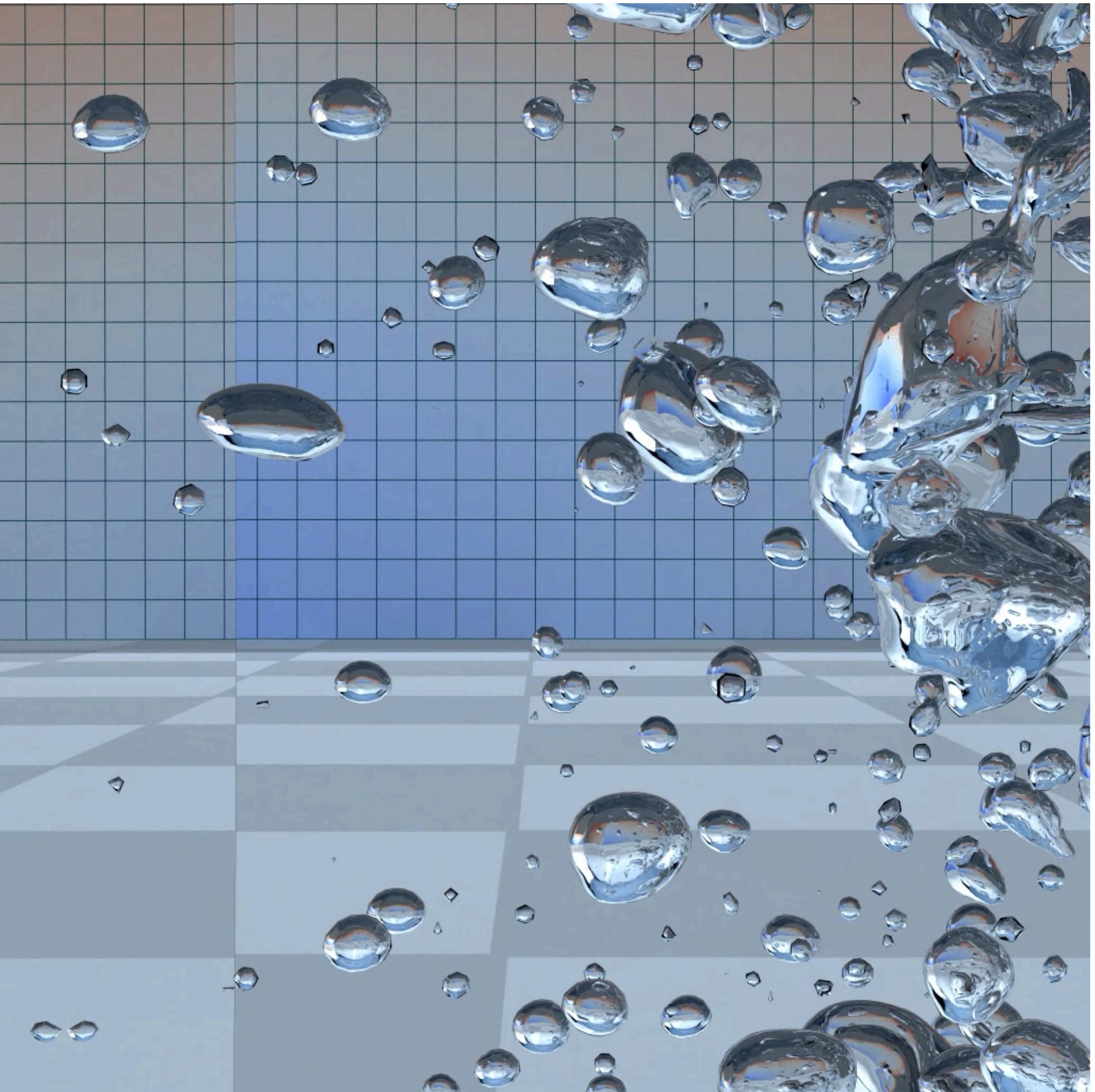
Visualization by Jean M. Favre (CSCS)  
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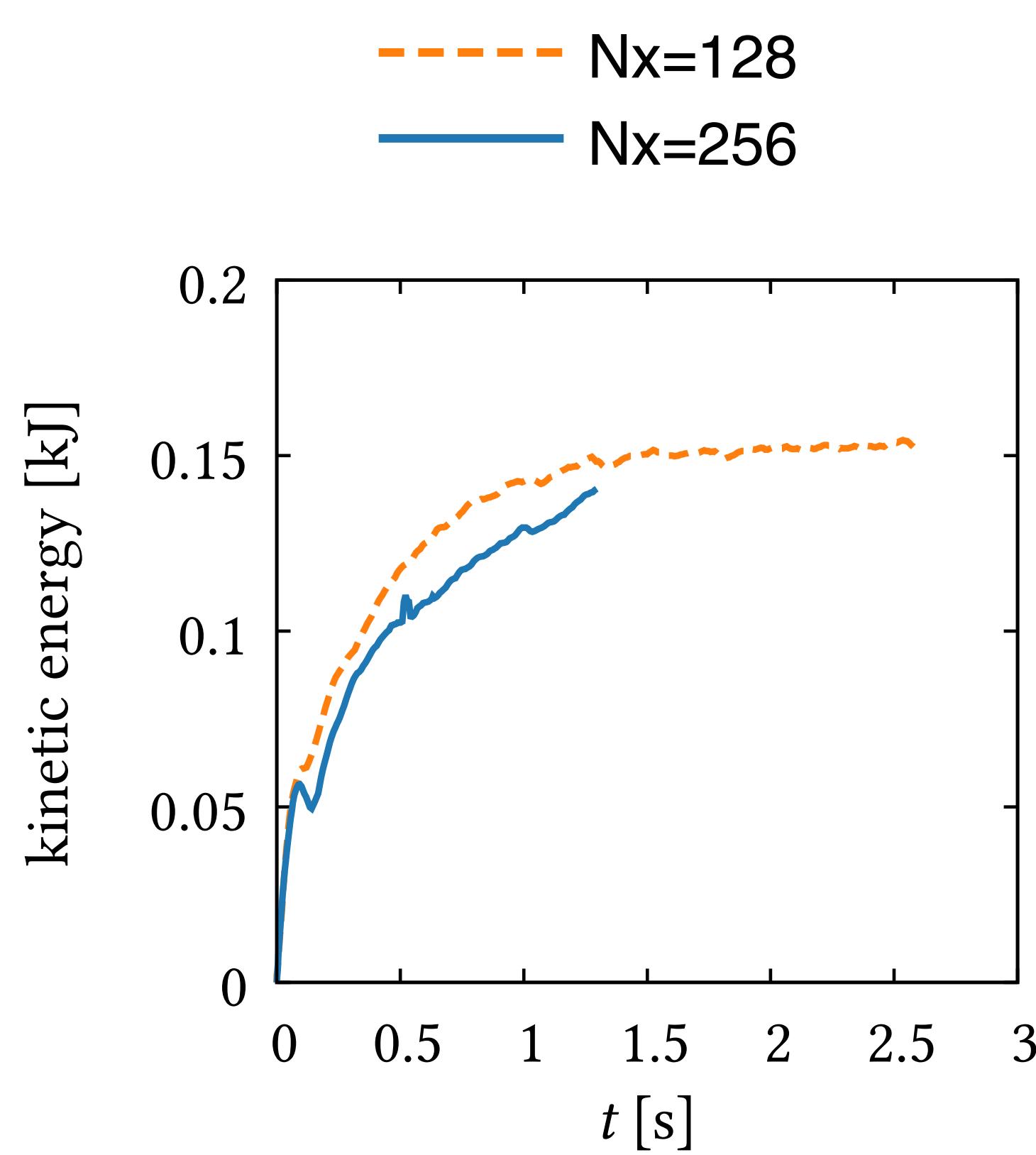
### 3. Rising bubbles

- larger bubbles are elliptical and follow zigzag trajectory

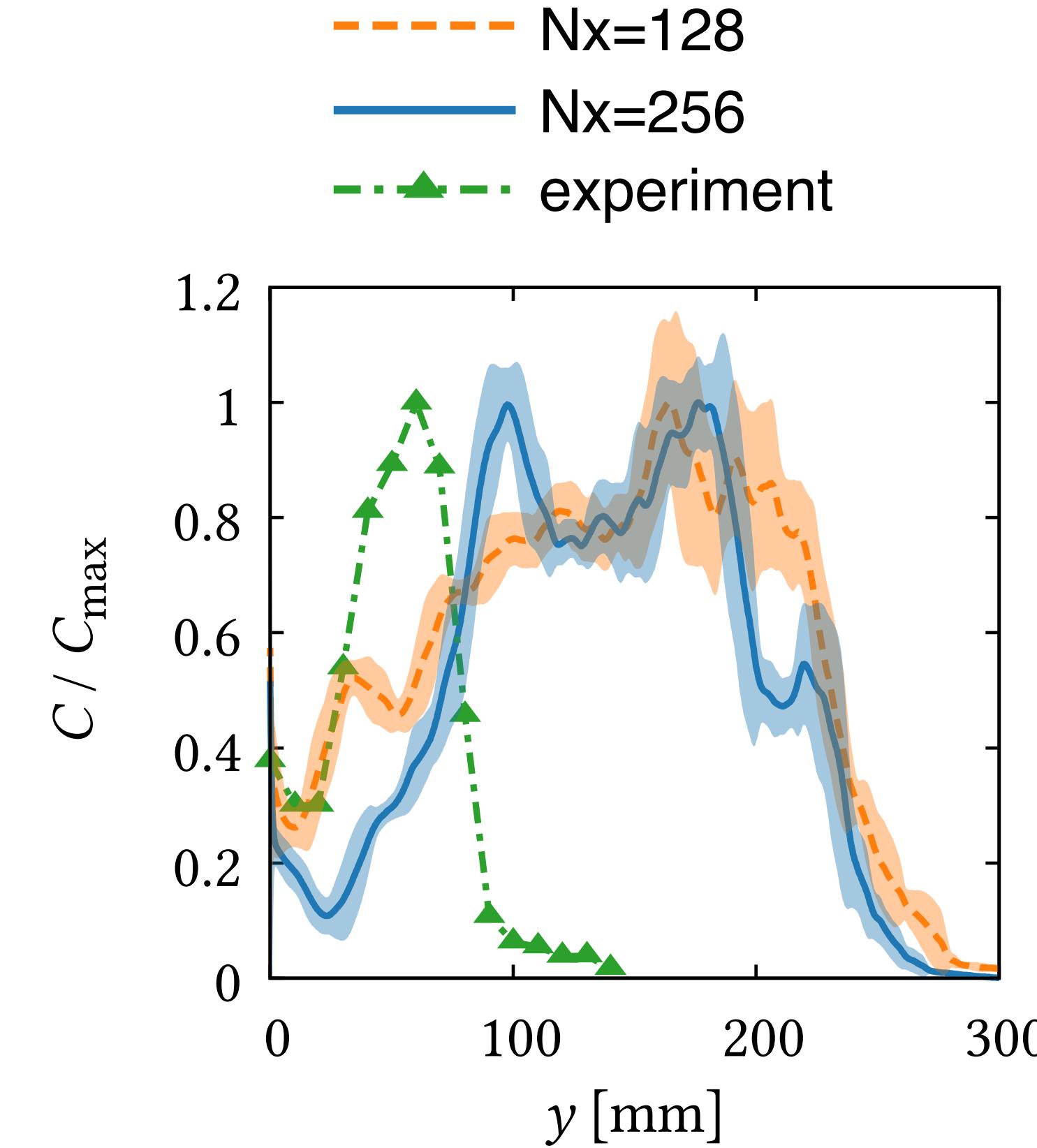
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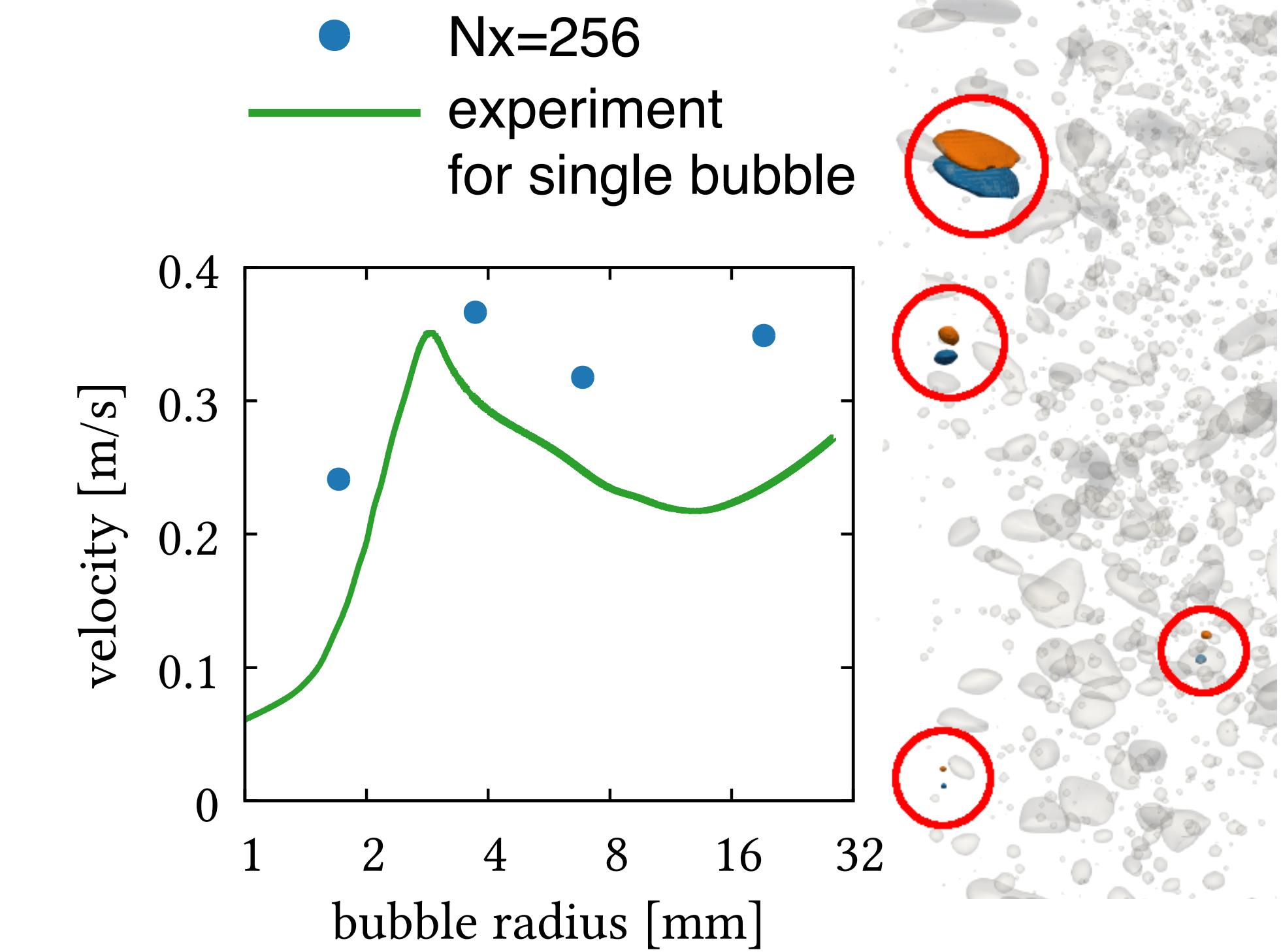
# Plunging jet with air entrainment



equilibration of  
mixture kinetic energy



axial concentration of gas,  
penetration depth overpredicted



velocity of selected bubbles  
compared to rise velocity  
of single bubble [Maxworthy 1996]

# Summary

- Particles for curvature estimation improve the accuracy at low resolution [arXiv:1906.00314]
- Bubbles of various scales are resolved on a uniform mesh
- Coroutines enable modularity with blockwise processing

## Outlook:

- performance kernels on GPU, compute-transfer overlap
- more applications turbulent multiphase flows
- open-source release

[tinyurl.com/demogrid](https://tinyurl.com/demogrid)

